

TITLE OF THE INVENTION

METHOD FOR PRODUCING NANO-CARBON MATERIALS

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BACKGROUND OF THE INVENTION1. Field of the Invention

The present invention relates to a method for producing nano-carbon materials. More particularly, the present invention relates to a method which enables one to quantitatively produce nano-carbon materials from relatively inexpensive starting material by a simple manner using a relatively inexpensive reaction apparatus. The nano-carbon materials produced according to the present invention include carbon nanotubes, carbon nanofibers, and the like.

2. Related Background Art

A fullerene C₆₀ having a soccer ball-like polyhedral molecular structure comprising 60 carbon atoms was discovered by H. W. Kroto, R. E. Smalley and R. F. Curl in 1985. Following the discovery of the fullerene C₆₀, a carbon nanotube (CNT) corresponding to a cylindrical molecule of a fullerene, specifically having a molecular structure in which a graphene sheet (a single atomic layer of crystalline graphite) rolled up into a cylinder was discovered by Iijima in 1991. Since then, other carbon nanotubes have been

discovered, and various studies on their industrial application have been carrying out.

And it has been reported that these carbon nanotubes have an excellent field emission performance, a
5 function to take up and store lithium therein and release said lithium in the electrochemical reaction, a large specific surface area and a good conductivity. In view of this, researches have been conducting to use these carbon nanotubes as electrode materials in FEDs
10 (field emission displays), as electrode materials in rechargeable lithium batteries, as catalyst-retaining materials in fuel cells in which polymer solid electrolytes are used, and as hydrogen storage materials in hydrogen storage systems.

15 As the method for producing such carbon nanotubes, there are known a method wherein arc-discharge is generated in an gas atmosphere containing a carbon material such as hydrocarbon, a method wherein a target comprising graphite is evaporated by irradiating a laser thereto, and a method
20 wherein a gaseous carbon material comprising acetylene or the like is subjected to thermal decomposition on a substrate having a catalyst of cobalt metal or nickel metal arranged thereon.

Particularly, Japanese Laid-open Patent Publication
25 6(1994)-157016 (hereinafter referred to as "Patent Document

1") discloses a method for producing carbon nanotubes, wherein arc-discharge is generated between a pair of carbon rods respectively as a positive electrode and a negative electrode in an inert gas atmosphere to deposit a carbon
5 nanotubes-containing solid material on the negative electrode.

Japanese Laid-open Patent Publication P2000-95509A (hereinafter referred to as "Patent Document 2") discloses a method for producing carbon nanotubes, wherein a rod-shaped
10 positive electrode containing carbon and non-magnetic transition metal and a rod-shaped negative electrode comprising graphite are arranged such that their tips are opposed to each other and arc-discharge is generated between the tip of the positive electrode and that of the negative electrode in an
15 inert gas atmosphere to deposit carbon nanotubes on the tip portion of the negative electrode.

Japanese Laid-open Patent Publication 9(1997)-188509 (hereinafter referred to as "Patent Document 3") discloses a method for producing carbon nanotubes, wherein a carbon
20 material and a metal catalyst are supplied into a high frequency plasma generated to deposit carbon nanotubes on a substrate.

Japanese Laid-open Patent Publication 10(1998)-273308 (hereinafter referred to as "Patent Document 4") discloses a method for producing carbon nanotubes, wherein a
25 graphite-containing carbon rod is positioned in a quartz tube

arranged in an electric furnace and a laser is irradiated to said carbon rod in an inert gas atmosphere to deposit carbon nanotubes on the inner wall face of the quartz tube.

Japanese Laid-open Patent Publication P2000-86217A
5 (hereinafter referred to as "Patent Document 5") discloses a method for producing carbon nanotubes, wherein gaseous hydrocarbon is thermally decomposed on a catalyst comprising a molybdenum metal or a molybdenum metal-containing material to deposit carbon nanotubes on said catalyst.

10 Separately, Carbon Vol. 36, No. 7-8, pp. 937-942, 1998 (Yury G. Gogotsi et al.) [hereinafter referred to as "Non-patent Document 1"] describes a method wherein filamentous carbons are formed from paraformaldehyde by way of hydrothermal reaction at a temperature of 700 to 750 °C under
15 100 Mpa pressure for 150 hours.

Journal of Materials Research Society, Vol. 15, No. 12, pp. 2591-2594, 2000 (Yury Gogosi et als.) [hereinafter referred to as "Non-patent Document 2"] describes a method wherein multiwall carbon nanotubes are formed from
20 polyethylene by way of pyrolysis of said polyethylene in the presence of nickel at a temperature of 700 to 800 °C under 100 Mpa.

Journal of American Chemical Society Vol. 123, No. 4, pp. 741-742, 2001 (Jose Maria Calderon et al.) [hereinafter
25 referred to as "Non-patent Document 3"] describes a method

wherein multiwall carbon nanotubes are formed from amorphous carbon by way of hydrothermal treatment of said amorphous carbon in the absence of a metal catalyst at a temperature of 800 °C under 100 Mpa pressure for 48 hours.

5 However, the methods disclosed in Patent Documents 1 to 5 have disadvantages such that the starting material and the apparatus used for practicing the method are costly and therefore a product obtained becomes unavoidably costly and it is difficult to quantitatively produce
10 nano-carbon materials.

 Similarly, the methods described in Non-patent Documents 1 to 3 have disadvantages such that because high pressure condition of 100 Mpa is adopted, a specific high pressure capsule made of Au (which is costly) and which can
15 withstand such high pressure is used as the reaction vessel, and the starting material and water are introduced into said capsule wherein the starting material is subjected to hydrothermal reaction at a high temperature (700 to 800 °C) under high pressure condition of 100 Mpa. Therefore, a
20 product obtained in any of these methods unavoidably becomes costly. And Non-patent Documents 1 to 3 do not even suggest a method wherein which nano-carbon materials (including carbon nanotubes or filamentous carbons) can be formed under low pressure condition of less than 60 Mpa,
25 using a relatively inexpensive pressure reaction vessel

without necessity of using such costly pressure reaction vessel.

There is a demand for providing a method capable of quantitatively producing nano-carbon materials (including carbon nanotubes and carbon nanofibers) at a reasonable production cost from relatively inexpensive raw material by a simple manner under low pressure condition which does not require to use such specific and costly pressure reaction vessel as above described.

10 Separately, Carbon Vol.40, pp. 2961-2973, 2002
(Mingwang Shao et als.) [hereinafter referred to as "Non-patent Document 4"] describes a method wherein carbon nanotubes having a multi-layered structure are formed by reacting benzene as a starting material with a nickel-iron powder
15 as a catalyst at a temperature of 480 °C under a reaction pressure of about 15 Pa pressure for 12 hours in a stainless steel autoclave. Although this method is advantageous in that the reaction pressure upon forming a nano-carbon material (a carbon nanotube having a
20 multi-layered structure) is low to be about 15 Pa, the method has a disadvantage in that the amount of a nano-carbon material produced in the reaction for a relatively long time of 12 hours is small, particularly a ratio of the weight of the nano-carbon material produced to the weight of the catalyst
25 used is 4.2 which is small. In addition, according to the

results of the measured Raman spectrum of the obtained nano-carbon material, which are described in Non-patent Document 4, it is understood that for the relative intensity between the so-called G-band peak near 1590 cm^{-1} due to
5 lattice vibration in the hexagonal lattice network of the carbon atoms and the so-called D-band peak near 1350 cm^{-1} due to lattice defect of the carbon atoms, the intensity of the peak near 1350 cm^{-1} is stronger. This means that the nano-carbon material obtained by the method described in
10 Non-patent Document 4 is accompanied by a number of lattice defects. Thus, although the method described in Non-patent Document 4 has an advantage in that the reaction pressure upon forming a nano-carbon material is low, it is difficult to stably produce a nano-carbon material whose lattice defect
15 is slight. It is desired for the method described in Non-patent Document 4 to be improved such that it can stably produce a high quality nano-carbon material with few lattice defect for a shortened reaction time.

By the way, such nano-carbon materials as above
20 described are expected to be widely used in various technical field, for instance, as electrode materials in FEDs (field emission displays), as electrode materials in rechargeable lithium batteries, and as catalyst-retaining materials in fuel cells. In view of this, there is a demand for
25 developing a technique which enables one to efficiently

produce high quality nano-carbon materials at a reasonable production cost.

SUMMARY OF THE INVENTION

The present invention has been accomplished in view
5 of the circumstances in the prior art for the production of nano-carbon materials.

The present invention makes it an object to provide a method which enables one to efficiently and quantitatively produce high quality nano-carbon materials,
10 which are effectively usable as electrode materials in FEDs (field emission displays), as electrode materials in rechargeable lithium batteries, and as catalyst-retaining materials in fuel cells, at a reasonable production cost from relatively inexpensive raw material by a simple
15 manner.

The method for producing nano-carbon materials in the present invention typically includes the following two embodiments.

A first embodiment that is characterized by
20 having a step (a) wherein (i) a starting material comprising one or more kinds of compounds selected from the group consisting saturated hydrocarbons, unsaturated hydrocarbons, saturated cyclic hydrocarbons, and alcohols whose atomic ratio of the component carbon to the component
25 oxygen is more than 2.0 and (ii) a catalyst comprising one

or more kinds of materials selected from the group consisting of transition metal element-containing materials, alumina, silica, and silicon carbides are together treated at a temperature in a range of from 100 to 800 °C while being
5 compressed at a pressure in a range of from 0.2 to 60 MPa, where said starting material is converted into a supercritical fluid or a subcritical fluid while said supercritical fluid or said subcritical fluid being contacted with said catalyst, thereby to obtain a reaction
10 product.

A second embodiment that is characterized by having a step (b) wherein (i) a starting material comprising one or more kinds of compounds selected from the group consisting saturated chain hydrocarbons, unsaturated chain hydrocarbons,
15 saturated cyclic hydrocarbons, and alcohols whose atomic ratio of the component carbon to the component oxygen is more than 2.0, (ii) a catalyst comprising one or more kinds of materials selected from the group consisting of transition metal element-containing materials, alumina, silica, and
20 silicon carbides and (iii) a supplementary material capable of functioning as a reaction promotion medium are together treated at a temperature in a range of from 100 to 800 °C while being compressed at a pressure in a range of from 0.2 to 60 MPa, where at least said supplementary material is
25 converted into a supercritical fluid or a subcritical

fluid and said starting material is contacted with said supercritical fluid or said subcritical fluid formed from said supplementary material while being contacted with said catalyst, thereby to obtain a reaction product.

5 The supercritical fluid means a fluid having liquid properties and gaseous properties and which is in a state with a temperature and a pressure respectively exceeding the critical point (the critical temperature and the critical pressure) where gas and liquid can together exist. The
10 subcritical fluid means a fluid following the supercritical fluid. Specifically, when the above critical temperature is made to be T_0 (absolute temperature) and the above critical pressure is made to be P_0 (MPa), the
15 subcritical fluid means a fluid which is in a state with an absolute temperature T and a pressure P which satisfy the following equations.

$$T \geq 0.8T_0$$

$$P \geq 0.8P_0$$

20 In the method of the present invention, it is preferred to make the pressure to fall in a range of from 2 to 40 Mpa. Similarly, it is preferred to make the temperature to fall in a range of from 200 to 650 °C.

25 In the method of the present invention in each of the first embodiment and the second embodiment, it is preferred that the starting material is in the liquid or

gaseous state in an atmosphere with normal temperature and normal pressure and has a dielectric constant in a range of from 1.5 to 25.0 at 25 °C.

In the method of the first embodiment in the present invention, it is possible that a supplementary material capable of functioning as a reaction promotion medium is made to coexist with the starting material which has been converted into said supercritical fluid or said subcritical fluid such that said supplementary material is contacted with said supercritical fluid or said subcritical fluid which are formed from said starting material, wherein said supplementary material comprises at least one kind of a material selected from the group consisting of a solvent to dissolve said starting material, a solvent to dissolve the catalyst, water, helium gas, argon gas, nitrogen gas, hydrogen gas, carbon monoxide, nitrous oxide, and ammonia.

Similarly, in the method of the first embodiment in the present invention, it is possible that a supplementary material capable of functioning as a reaction promotion medium is made to coexist with the starting material which is converted into said supercritical fluid or said subcritical fluid such that said supplementary material is contacted with said starting material, wherein said supplementary material comprising at least one kind

of a material selected from the group consisting of a solvent to dissolve said starting material, a solvent to dissolve the catalyst, water, helium gas, argon gas, nitrogen gas, hydrogen gas, carbon monoxide, nitrous oxide, and ammonia.

The solvent to dissolve the starting material is preferred to comprise at least one kind of a material selected from the group consisting of carbon dioxide, aromatic hydrocarbons, and ethers.

The transition metal element of the transition metal element-containing material as the catalyst is preferred to be a transition element selected from the group consisting of Ni, Co, Fe, Cu, Ag, Cr, W, Mo, Ti, Ru, Rh, and Pd.

The transition metal element-containing material may comprise at least one kind of a transition metal selected from the group consisting of transition metals of aforesaid transition metal elements or at least one kind of a transition metal compound selected from the group consisting of transition metal compounds of these transition metal elements.

The transition metal compound can include transition metal sulfides, transition metal carbides, organo transition metal compounds, transition metal nitrides, transition metal oxides, and salts of transition metals.

These transition metal compounds may be used either singly or in combination of two or more of them.

In the method of each of the first embodiment and the second embodiment in the present invention, in the case
5 where a transition metal element-containing material is used as the catalyst, it is possible that a surfactant is made to coexist with said transition metal element-containing material.

In the method of each of the first embodiment and
10 the second embodiment in the present invention, there is afforded a reaction product containing nano-carbon materials.

The method of each of the first embodiment and the second embodiment in the present invention further includes
15 a step of subjecting the reaction product to a heat treatment at a temperature in a range of from 400 to 2800 °C, in order to remove impurities including amorphous carbons contained in the nano-carbon materials and to make the nano-carbon materials have an improved crystallinity. In
20 the case where the graphitization is insufficient, it is preferred that the heat treatment is performed at a temperature in a range of from 600 to 2200 °C. In a preferred embodiment, the heat-treating step is performed in such a way that the reaction product is subjected to a first heat
25 treatment at a temperature in a range of from 400 to 900 °C,

then, the reaction product is subjected to a second heat treatment at a temperature in a range of from 900 to 2800 °C.

The heat treatment in the heat-treating step is preferred to be performed in a gas atmosphere composed of
5 one or more gases selected from the group consisting of argon gas, helium gas and nitrogen gas.

The method of each of the first embodiment and the second embodiment in the present invention is preferred to include a purification step in that the heated-treated
10 product is purified. Specifically, in the case where the nano-carbon materials contained in the heat-treated reaction product contain a magnetic metal element therein resulted from the catalyst, the magnetic metal element-containing nano-carbon materials are collected by
15 means of a magnet, whereby it is possible to obtain a purified nano-carbon materials-containing product.

Separately, in the case where the nano-carbon materials contain a transition metal or a transition metal compound resulted from the catalyst and it is not necessary for the
20 nano-carbon materials to contain such transition metal or such transition metal compound, it is possible to remove such transition metal or such transition metal compound therefrom by way of washing with an acid or the like.

The nano-carbon materials produced according to
25 the method of the present invention are somewhat different

depending the related conditions including the kind of the starting material used, the kind of the catalyst used, the kind of the supplementary material as the reaction promotion medium used to form a supercritical fluid or a subcritical fluid
5 to be contacted with the starting material, and the temperature and the pressure adopted in the synthesis reaction.

However, the nano-carbon materials produced according to the method of the present invention include nano-carbon materials comprising such aggregates as
10 below-mentioned which are identified by a scanning electron microscope (SEM). Particularly, the nano-carbon materials produced according to the method of the present invention typically include nano-carbon materials comprising aggregates of a plurality of filament-like shaped
15 (or worm-like shaped) microunits, and nano-carbon materials comprising aggregates of a plurality of tube-like shaped microunits, wherein the microunits in each case have an average diameter in a range of from 4 to 400 nm and an average length in a range of from 100 to 10000 nm. In the
20 method of the present invention, these filament-like (or worm-like) or tube-like nano-carbon materials are likely to be produced at a desirably high purity. And the diameters of these nonocarbon materials are liable to depend on the average particle size of a powdery catalyst used as the
25 catalyst in the method of the present invention.

According to observation by a transmission electron microscope (TEM) with respect to aforesaid microunits, the nano-carbon materials produced according to the method of the present invention include (a) nano-carbon materials
5 having a microstructure in that a plurality of graphene sheets shaped in a cup-like or megaphone-like form which are stacked and developed into a filament-like state, (b) nano-carbon materials having a microstructure in that a graphene sheet is wound in a lengthwise direction
10 parallel to or slant to a fiber axis into a single-layered tubular form or a multi-layered tubular form, (c) nano-carbon materials comprising a platelet type graphite nanofiber in which a plurality of graphene sheets are stacked vertically to a fiber axis or a
15 herring-bone type graphite nanofiber in which a plurality of graphene sheets are stacked slantingly to a fiber axis, and (d) nano-carbon materials having a microstructure in that a graphene sheet is developed into a sphere form or a disk form.

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 shows a flow chart illustrating an example of the method for producing nano-carbon materials in the present invention..

FIG. 2 is a schematic cross-sectional view
25 illustrating an example of a reaction apparatus used for

producing nano-carbon materials according to the method of the present invention.

FIG. 3 is a schematic cross-sectional view illustrating another example of a reaction apparatus used for producing nano-carbon materials according to the method of the present invention.

FIG. 4 is a schematic cross-sectional view illustrating an example of a rechargeable lithium battery in which a nano-carbon material obtained according to the method of the present invention is applied.

FIG. 5 is a schematic cross-sectional view illustrating an example of an electrode structural body for a rechargeable lithium battery, wherein said electrode structural body is formed using a nano-carbon material obtained according to the method of the present invention.

FIG. 6 is a schematic cross-sectional view illustrating an example of a FED in which a nano-carbon material obtained according to the method of the present invention is applied.

FIG. 7 is a schematic cross-sectional view illustrating an example of an element for examining the field emission performance of a nano-carbon material.

FIG. 8 is a schematic diagram illustrating an example of an apparatus for examining the hydrogen-storing performance of a nano-carbon material.

FIG. 9 shows a SEM (scanning electron microscope) image of a nano-carbon material produced according to the method of the present invention in Example 1 which will be described later.

5 FIG. 10 shows a TEM (transmission electron microscope) image (observed at a low magnification) of a nano-carbon material produced according to the method of the present invention in Example 1 which will be described later.

10 FIG. 11 shows another TEM image (observed at a high magnification) of a nano-carbon material produced by the method of the present invention in Example 1 which will be described later.

 FIG. 12 is a schematic view illustrating a conjectured unit structure of an example of a
15 filament-like nano-carbon material produced according to the method of the present invention.

 FIGs. 13(a) to 13(e) are schematic views respectively illustrating a microstructure inferred from a TEM image of a nano-carbon material produced according to the method of the
20 present invention.

 FIG. 14 shows a TEM image of a nano-carbon material produced according to the method of the present invention in Example 10 which will be described later.

 FIG. 15 shows a SEM image of a nano-carbon
25 material produced by the method of the present invention in

Example 11 which will be described later.

FIG. 16 shows a SEM image of a nano-carbon material produced by the method of the present invention in Example 12 which will be described later.

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DETAILED DESCRIPTION OF THE INVENTION AND
PREFERRED EMBODIMENTS

As previously described, the present invention provides a method which enables one to quantitatively produce nano-carbon materials. The method for producing
10 nano-carbon materials in the present invention typically includes the following two embodiments.

A first embodiment that is characterized by having a step (a) wherein (i) a starting material comprising one or more kinds of compounds selected from the group
15 consisting saturated hydrocarbons, unsaturated hydrocarbons, saturated cyclic hydrocarbons, and alcohols whose atomic ratio of the component carbon to the component oxygen is more than 2.0 and (ii) a catalyst comprising one or more kinds of materials selected from the group
20 consisting of transition metal element-containing materials, alumina, silica, and silicon carbides are together treated at a temperature in a range of from 100 to 800 °C while being compressed at a pressure in a range of from 0.2 to 60 MPa, where said starting material is converted into a
25 supercritical fluid or a subcritical fluid while said

supercritical fluid or said subcritical fluid being contacted with said catalyst, thereby to obtain a reaction product.

A second embodiment that is characterized by having
5 a step (b) wherein (i) a starting material comprising one or more kinds of compounds selected from the group consisting saturated hydrocarbons, unsaturated hydrocarbons, saturated cyclic hydrocarbons, and alcohols whose atomic ratio of the component carbon to the component oxygen is more than 2.0, (ii)
10 a catalyst comprising one or more kinds of materials selected from the group consisting of transition metal element-containing materials, alumina, silica, and silicon carbides, and (iii) a supplementary material capable of functioning as a reaction promotion medium are together
15 treated at a temperature in a range of from 100 to 800 °C while being compressed at a pressure in a range of from 0.2 to 60 MPa, where at least said supplementary material is converted into a supercritical fluid or a subcritical fluid and said starting material is contacted with said supercritical
20 fluid or said subcritical fluid formed from said supplementary material while being contacted with said catalyst, thereby to obtain a reaction product. In this case, it is possible that said starting material is also converted into a supercritical fluid or a subcritical
25 fluid. Said supplementary material comprises at least one

kind of a material selected from the group consisting of a solvent to dissolve said starting material, a solvent to dissolve the catalyst, water, helium gas, argon gas, nitrogen gas, hydrogen gas, carbon monoxide, nitrous oxide, and ammonia.

As specific preferable examples of the saturated hydrocarbon used as the starting material, there can be mentioned methane, ethane, propane, butane, pentane, hexane, heptane, octane, nonane, decane, undecane, dodecane, tridecane, tetradecane, pentadecane, hexadecane, heptadecane, octadecane, nonadecane, eicosane, isobutene, dimethylbutane, trimethylpentane, methyloctane, methylheptane, and methylpentane. These saturated chain hydrocarbons may be used either singly or in combination of two or more of them.

Of these saturated hydrocarbons, pentane, hexane, heptane, octane, nonane, decane, undecane, dodecane, tridecane, pentadecane, hexadecane, heptadecane, octadecane, and nonadecane are more preferable, because these are in the liquid or solid state in an atmosphere with normal temperature and normal pressure and can be easily handled. And in terms of acquisition cost, n-hexane and methane are preferable because they can be readily acquired at a reasonable cost.

As specific preferable examples of the unsaturated hydrocarbon used as the starting material, there can be

mentioned ethylene, propene (propylene), butane, pentene, hexene, heptene, octene, nonene, decene, methylpropene, cyclohexene, cyclopentene, butadiene, propadiene, acetylene, and propyne. These unsaturated hydrocarbons can be used
5 either singly or in combination of two or more of them.

Of these unsaturated hydrocarbons, ethylene, propene, and butadiene are more preferable because they can be readily acquired at a reasonable cost and they are high in terms of conversion efficiency into nano-carbon
10 material.

As specific preferable examples of the saturated cyclic hydrocarbon used as the starting material, there can be mentioned cyclopropane, cyclobutane, cyclopentane, cyclohexane, cycloheptane, cyclooctane, cyclononane,
15 cyclodecane, methylcyclohexane, methylcyclopentane, dimethylcyclopentane, and decalin. These saturated cyclic hydrocarbons can be used either singly or in combination of two or more of them.

As specific preferable examples of the alcohol
20 whose atomic ratio of the component carbon to the component oxygen is more than 2.0 used as the starting material, there can be mentioned ethanol, propanol, butanol, pentanol, hexanol, heptanol, octanol, nonanol, decanol, undecanol, dodecanol, tridecanol, tetradecanol, pentadecanol, hexadecanol,
25 heptadecanol, octadecanol, isobutyl alcohol, propanol,

t-butanol, methylbutanol, pentanol, cyclohexanol, and allyl alcohol. These alcohols can be used either singly or in combination of two or more of them.

Of these alcohols, propanol and butanol are more
5 preferable because they can be readily acquired at a reasonable cost and they are high in terms of conversion efficiency into nano-carbon material.

Besides those mentioned in the above, a liquefied natural gas containing methane as a main component and
10 ethane, propane, butane, nitrogen, carbon dioxide, and sulfur compound and a liquefied petroleum gas comprising a mixture composed of propane, propylene, n-butane, isobutene, butylene, and isobutylene can be used as the starting material. To use the liquefied natural gas or the liquefied
15 petroleum gas is advantageous because they are relatively inexpensive.

However, of those materials mentioned in the above as the starting material, the unsaturated hydrocarbons are the most appropriate in a viewpoint that they are desirably
20 high in terms of conversion efficiency into nano-carbon material. For the reason why the unsaturated hydrocarbons are desirably high in terms of conversion efficiency into nano-carbon material, it is considered such that they are inherently liable to cause polymerization reaction and
25 because of this, when contacted with the catalyst at a

temperature in a range of from 100 to 800 °C and at a pressure in a range of from 0.2 to 60 MPa, C=C bonds are readily formed to afford nano-carbon materials.

In order to make it possible that a reaction product is readily separated from the unreacted remainder of the starting material, it is more preferred that the starting material is in the liquid or gaseous state in an atmosphere with normal temperature and normal pressure. However, in terms of easiness in the handling, the starting material is more preferred to be in the liquid state. And in terms of easiness in the separation of a reaction product from the unreacted remainder of the starting material, the starting material is more preferred in the gaseous state.

In order that the preparation work can be easily carried out and that the separation of the reaction product from the unreacted remainder of the starting material can be readily performed, it is possible to take a manner wherein the starting material in the gaseous state in an atmosphere with normal temperature and normal pressure is liquefied or solidified by cooling said starting material, followed by being introduced into a reaction vessel.

The previously illustrated saturated hydrocarbons, unsaturated hydrocarbons, saturated cyclic hydrocarbons, and alcohols whose atomic ratio of the component carbon to the component oxygen is more than 2.0 as

the starting material may be used either singly or in combination of two or more of them. It is possible to use an aromatic compound in combination with one of these materials or a mixture comprising two or more of these materials.

5 Such aromatic compound can include benzene, ethylbenzene, butylbenzene, toluene, xylene, styrene, biphenyl, phenylacetylene, phenol, ethylphenol, fluoranthene, pyrene, chrysene, phenanthrene, anthracene, naphthalene, methylnaphthalene, and fluorene, acenaphthene. Besides,
10 pitch, pitch coke, petroleum coke, and coal tar which are aromatic compound-containing materials may be used instead of the aromatic compound.

Now, the starting material used in the method of the present invention is converted into a supercritical fluid or
15 a subcritical fluid under condition with a temperature in a range of from 100 to 800 °C and a pressure in a range of from 0.2 to 60 MPa in the presence of the catalyst.

Here, the critical temperature and the critical pressure at which hexane belonging to the saturated
20 hydrocarbon as the starting material is converted into a supercritical fluid are respectively 234.4 °C and 2.97 MPa. The critical temperature and the critical pressure at which methane belonging to the saturated hydrocarbon as the starting material is converted into a supercritical fluid are
25 respectively -82.45 °C and 4.95 MPa. Separately, the critical

temperature and the critical pressure at which ethylene belonging to the unsaturated hydrocarbon as the starting material is converted into a supercritical fluid are respectively 9.65 °C and 5.076 MPa. The critical temperature and the critical pressure at which propylene belonging to the unsaturated hydrocarbon as the starting material is converted into a supercritical fluid are respectively 92 °C and 4.62 MPa. The critical temperature and the critical pressure at which acetylene belonging to the unsaturated hydrocarbon as the starting material is converted into a supercritical fluid are respectively 35.33 °C and 6.139 MPa. The critical temperature and the critical pressure at which 1-butanol belonging to the alcohol whose atomic ratio of the component carbon to the component oxygen is more than 2.0 as the starting material is converted into a supercritical fluid are respectively 289.93 °C and 4.413 MPa.

Now, in terms of easiness in the handling, it is advantageous that the starting material has a boiling point which is higher than 30 °C and is in the liquid or solid state under room temperature condition, and in terms of easiness in the separation of a reaction product from the unreacted remainder of the starting material, it is advantageous that the starting material is in the gaseous or solid state under room temperature condition.

As previously described, the starting material may be

singly used. However, it is possible to use the starting material together with other appropriate material.

As such other appropriate material, it is preferred to use a material capable of functioning as a medium (a reaction
5 promotion medium) to promote the synthesis reaction to form nonacarbon materials from the starting material when said material in an ordinary state (yet having converted into a supercritical or subcritical fluid state) is contacted with the starting material, when said material having
10 converted into a supercritical or subcritical state is contacted with the starting material yet having converted into a supercritical or subcritical fluid state, or when said material having converted into a supercritical or subcritical fluid state is contacted with the starting
15 material having converted into a supercritical or subcritical fluid state.

In any of these cases, it is more preferred that said material comprises a solvent for the starting material. In the case where in addition to the starting material, a
20 solvent for the starting material is used in the formation of nano-carbon materials from the starting material, it is preferred for the starting material to have a dielectric constant in a range of from 1.5 to 25.0, in order that the starting material and the solvent are uniformly mixed with
25 each other.

As previously described, the supercritical fluid used in the present invention means a fluid having liquid properties and gaseous properties and which is in a state with a temperature and a pressure respectively exceeding the
5 critical point (the critical temperature and the critical pressure) where gas and liquid can together exist. And the subcritical fluid used in the present invention means a fluid following the supercritical fluid. Specifically, when the above critical temperature is made to be T_0 (absolute
10 temperature) and the above critical pressure is made to be P_0 (MPa), the subcritical fluid means a fluid which is in a state with an absolute temperature T and a pressure P which satisfy the following equations.

$$T \geq 0.8T_0$$

15 $P \geq 0.8P_0$

The reaction to form nano-carbon materials in the method of the present invention may be performed, for instance, in the following manner.

The starting material and the catalyst, and if
20 necessary, such reaction promotion medium as described in the above are introduced into a substantially enclosed pressure reaction vessel, and the starting material, the catalyst and the reaction promotion medium introduced into the reaction vessel are together heated while being
25 compressed under condition with a prescribed temperature

and a prescribed pressure where the starting material is converted into a supercritical fluid or a subcritical fluid, wherein the starting material (which is converted into said supercritical fluid or said subcritical fluid) is contacted with the catalyst and the reaction promotion medium to cause reaction of the starting material, whereby nano-carbon materials are synthesized.

In the alternative, the reaction to form nano-carbon materials in the method of the present invention may be performed in the following manner.

The starting material, the catalyst and a given reaction promotion medium capable of forming a supercritical fluid or a subcritical fluid are introduced into the pressure reaction vessel, and the starting material, the catalyst and the reaction promotion medium introduced in the reaction vessel are together heated while being compressed under condition with a prescribed temperature and a prescribed pressure where the reaction promotion medium is converted into a supercritical fluid or a subcritical fluid, wherein the starting material is contacted with said supercritical fluid or said subcritical fluid formed from said reaction promotion medium and also contacted with the catalyst to cause reaction of the starting material, whereby nano-carbon materials are synthesized. In this

case, it is possible that the starting material itself is converted into a supercritical fluid or a subcritical fluid at the same time of converting the reaction promotion medium into the supercritical fluid or the subcritical fluid.

The heating temperature and the compressing pressure in the above are somewhat different depending upon the kind of the material used for forming the supercritical fluid or the subcritical fluid. However, in general, it is desirable that the heating temperature is made to fall in a range of from 100 to 800 °C and the compressing pressure is made to fall in a range of from 0.2 to 60 MPa in terms of easiness in the reaction, suppression of a raise in the cost of the apparatus used, and reduction in the operation energy. And in terms of an increase in the yield of a nano-carbon material, suppression of a raise in the cost of the apparatus used, and diminution in the operation energy, it is desirable that the heating temperature is made to fall preferably in a range of from 300 to 800 °C or more preferably in a range of from 300 to 650 °C and the compressing pressure is made to fall in a range of from 2 to 30 MPa.

In the method of the present invention, it is preferred that not only the starting material but also other materials which are used for synthesizing nano-carbon

materials are respectively in a supercritical fluid state, because the reaction velocity of synthesizing nano-carbon materials is increased in this case. Here, the critical pressure of the starting material used in the method of the present invention is more than 1.1 MPa.

Now, the catalyst used in the method of the present invention is preferred to be in a powdery form. In the case where a given transition metal element-containing material in a powdery form is used as the catalyst, when the transition metal element-containing material is contacted with air during the handling or when it is contacted with oxygen in the reaction vessel, a transition metal oxide film such as a nickel oxide film, a cobalt oxide film or an iron oxide film is liable to form so as to cover the surface of the transition metal element-containing material. It is necessary that the surface of the transition metal element-containing material which is covered with such transition metal oxide film is exposed by being reduced with hydrogen or carbon monoxide generated during the reaction in the reaction vessel. Here, the reduction of nickel oxide, cobalt oxide and iron oxide with hydrogen or carbon monoxide is started from about 200 °C. Therefore, in the case where the transition metal element-containing material is used as the catalyst, it is preferred that the reaction to produce

nano-carbon materials in the reaction vessel is performed at a temperature of 300 °C or more.

In the method of the present invention, in the case where a supplementary material capable of forming a
5 supercritical fluid or a subcritical fluid is used other than the starting material, said supplementary material is preferred to comprise at least one kind of a material selected from the group consisting of a solvent to dissolve the starting material, a solvent to dissolve the
10 catalyst, water, helium gas, argon gas, nitrogen gas, hydrogen gas, carbon monoxide, nitrous oxide, and ammonia.

It is considered that these supplementary materials function as a reaction promotion medium to promote the synthesis reaction to form nonacarbon materials from the
15 starting material. The dielectric constant of the supercritical fluid or the subcritical fluid which are formed from any of aforesaid supplementary materials is relatively low, and that of the starting material is also relatively low as previously described. In view of this, it
20 is considered that the supercritical fluid or the subcritical fluid which are formed from any of aforesaid supplementary materials becomes to be a good solvent for the starting material. In this connection, in the case where the supplementary material is used, it is preferred that the
25 heating temperature and the compression pressure in the

method of the present invention exceed the critical temperature and the critical pressure of the supplementary material.

In the case where the starting material itself has
5 been converted into a supercritical fluid or a subcritical fluid, it is in a very active state where reaction is liable to readily occur. Upon the synthesis of nonocarbon materials according to the method of the present invention, it is preferred that not only the fluid of the starting
10 material but also the fluids of other materials used for the synthesis of nonocarbon materials are in a supercritical state.

In the method of the present invention, it is preferred that not only the starting material but also the
15 reaction promotion medium (the foregoing supplementary material) comprise a material capable of being converted into a supercritical fluid under condition with a temperature in a range of from 100 to 800 °C and a pressure in a range of from 0.2 to 60 Ma.

20 Now, as previously described, the catalyst used in the method of the present invention is preferred to be in a powdery form.

The sizes of nano-carbon materials synthesized are quite liable to greatly depend on the particle sizes
25 of the catalyst in a powdery form. In order to obtain

nano-carbon materials which are substantially uniform with respect to their sizes, it is necessary that the catalyst is finely powdered to comprise fine particles and the catalyst fine particles are sufficiently contacted with
5 the starting material such that each of the catalyst fine particles is contacted with the starting material. In this respect, it is preferred that a solvent capable of dissolving the starting material or/and the catalyst (the catalyst fine particles) is mixed with the starting material
10 and the catalyst. Separately, in order to desirably disperse the catalyst fine particles in a state in that they are not aggregated, it is preferred to add a surfactant to the solvent.

As specific examples of such solvent to dissolve the starting material or/and the catalyst, there can be
15 illustrated carbon dioxide, water, alcohols, ethers, and aromatic compounds such as toluene and benzene. These solvents may be used either singly or in combination of two or more of them as a mixed solvent. As specific examples of said alcohol, there can be illustrated methanol,
20 ethanol, and propyl alcohol.

Of the above-mentioned solvents, carbon dioxide is the most appropriate for the reasons that besides functioning as the solvent, carbon dioxide itself is poor in terms of the reactivity and because of this, it is presumed
25 that carbon dioxide will function to reduce the probability

for the molecules of the starting material to be mutually collided and prevent side reactions from being occurred.

Here, the critical temperature and the critical pressure at which carbon dioxide is converted into a supercritical fluid are respectively 31 °C and 7.4 MPa. The critical temperature and the critical pressure at which water is converted into a supercritical fluid are respectively 374 °C and 22.0 MPa. And the critical temperature and the critical pressure at which toluene belonging to the aromatic compound is converted into a supercritical fluid are respectively 319 °C and 4.11 MPa.

In the method of the present invention, it is possible to introduce inert gas into the reaction system in order to synthesize nano-carbon materials at a high purity while reducing the probability for the molecules of the starting material to be mutually collided and preventing side reactions from being occurred. As such inert gas, argon gas, helium gas, or nitrogen gas may be used. Separately, hydrogen gas is generated when the starting material is decomposed in the reaction system. This hydrogen gas has a reduction action and an etching action. Because of this, it is considered that said hydrogen gas functions to maintain the surface of the catalyst in an active state, to prevent occurrence of side reactions of forming amorphous carbon which is structurally unstable, and to promote the growth of

only strong and stable nano-carbon networks.

In the method of the present invention, when the starting material is converted into a supercritical fluid or a subcritical fluid and it is contacted with a given catalyst (comprising one or more kinds of materials selected from the group consisting of transition element-containing materials, silica, silicon carbide, and alumina), if necessary in the presence of a supercritical fluid or a subcritical fluid formed from the foregoing supplementary material as the reaction promotion medium, said catalyst functions as a starting point to initiate formation of nano-carbon materials from the starting material and the nano-carbon materials thus started forming are gradually grown. In this, it is considered that the transition metal element-containing material, alumina, silica or silicon carbide behaves like a catalyst. It is possible that a composite comprising a given transition metal retained on a silica, a zeolite or an alumina is used as the catalyst.

In the case where a given transition metal element-containing material capable of being maintained in such a metal state that the valence number of the transition metal element becomes to be zero during the reaction of synthesizing nano-carbon materials is used as the catalyst, filament-like nano-carbon materials are produced in a very large amount. As such transition metal

element-containing material, there can be mentioned transition metal powders, composites comprising a transition metal retained on a carrier having a large specific surface area, and organo transition metal
5 compounds capable of affording a transition metal fine power when thermally decomposed.

Now, any of such catalysts as above described is introduced into the reaction vessel together with the starting material and if necessary, the supplementary material as the
10 reaction promotion medium, where when the starting material or the reaction promotion medium is converted into a supercritical fluid or a subcritical fluid, the catalyst is made to conduct with said supercritical fluid or said subcritical fluid. The catalyst is not always necessary to
15 be externally added. The catalyst may be a transition metal or a transition metal compound which are originally contained in the starting material or which are resulted when the starting material is converted into the supercritical fluid or the subcritical fluid or
20 contacted with the supercritical fluid or the subcritical fluid formed from the reaction promotion medium. Or the constituent components of the reaction vessel may be used as the catalyst. It is possible to used plural kinds of these catalysts.

25 As such transition metal element-containing

material, there can be illustrated transition metals, and transition metal compounds. Besides, there can be also illustrate composites comprising a transition metal element retained on a carrier comprising an oxide material having a large specific surface area such as silica or zeolite. In this case, it is possible that two or more kinds of transition metal elements are retained said carrier. The carrier in this case is not limited such oxide material. It is possible to used a carbon material having a large specific area such as activated carbon or the like.

The transition metal element of the transition element-containing material used as the catalyst in the method of the present invention can include Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Y, Zr, Nb, Mo, Ru, Rh, Pd, Ag, Ta, W, Pt, and Au. Of these, Ni, Co, Fe, Cu, Cr, W, Mo, Ti, V, Mn, Ru, Rh, Pd, and Ag are more preferred, and Ni, Co, Fe, Cu, Cr, W, Mo, and Ti are most preferred.

The transition metal element-containing material may comprise at least one kinds of a transition metal selected from the group consisting of transition metals of these transition metal elements or at least one kind of a transition metal compound selected from the group consisting of transition metal compounds of these transition metal elements.

The transition metal compound can include transition

metal oxides, transition metal hydroxides, organo
transition metal compounds, transition metal sulfides,
transition metal carbides, transition metal nitrides, and
salts of transition metal elements (hereinafter referred to
5 as transition metal salts).

The organo transition metal compounds mentioned
in the above are preferable for the reason that any of them
is easily decomposed to form a transition metal fine powder
when the starting material is decomposed under the high
10 temperature-high pressure condition and said transition
metal fine powder functions as the catalyst in the
synthesis reaction in the method of the present invention,
although they are relatively costly.

The above-mentioned transition metal oxides,
15 transition metal hydroxides, and transition metal salts are
preferable for the reason that any of them is reduced with
hydrogen gas generated when the starting material is
decomposed under the high temperature-high pressure
condition, to form a transition metal powder and said
20 transition metal powder functions as the catalyst in the
synthesis reaction in the method of the present invention.

The above-mentioned transition metal salts are
preferable for the reason that any of them is reduced or
oxidized in the synthesis reaction in the method of the
25 present invention to convert into a transition metal or a

transition metal oxide, where said transition metal or said transition metal oxide can be recovered as a transition metal salt by dissolving with an acid. The transition metal salt recovered in this way can be recycled to use as the catalyst
5 in the method of the present invention. However, in the case where the transition metal salt is a transition metal nitrate or a transition metal sulfate, these transition metal salts are liable to generate oxygen. Therefore, it is not preferable that these transition metal salts are singly used.

10 As preferable specific examples of aforesaid organo transition metal compound, there can be illustrated ferrocene, nickelocene, nickel formate, nickel oxalate, nickel naphthenate, nickel phthalocyanine, cobalt phthalocyanine, copper phthalocyanine, nickel acetylacetonato,
15 cobalt acetylacetonato, iron acetylacetonato, copper acetylacetonato, nickel carbonyl, cobalt carbonyl, iron carbonyl, bis(triphenylphosphine)dicarbonylnickel, dibromobis(triphenylphosphine)nickel, and chlorotris(triphenylphosphine)rhodium.

20 The carbon element contained in these organo transition metal compounds occasionally becomes to constitute a part of nano-carbon materials formed in the synthesis reaction in the method of the present invention.

Here, the catalyst used in the method of the present
25 invention includes decomposed products produced in the

synthesis reaction in the method of the present invention which exhibit a catalytic action

As previously described, as the catalyst used in the method of the present invention, it is preferred to use a
5 powdery catalyst.

In the case where the average diameter of microunits (observed in the observation by the electron microscope) which constitute nano-carbon materials produced according to the method of the present invention depends on
10 the average particle size of the catalyst particles, it is important to properly control the average particle size of the catalyst particles.

In order to obtain nano-carbon materials whose diameters are small and which are substantially uniform
15 with respect to their sizes, it is preferred to adopt (i) a manner in that the catalyst particles are used by dispersing them in a carrier having a large specific surface area so as to retain them on the carrier or (ii) a
manner in that in addition to the catalyst particles, a
20 solvent capable of dissolving them is introduced or a surfactant capable of preventing them from being aggregated is introduced.

In the present invention, in order to more promote the synthesis of nano-carbon materials, it is possible that
25 one or more kinds of materials selected from the group

consisting of sulfur and sulfur compounds are made to coexist with the transition metal or the transition metal compound as the transition metal element-containing material as the catalyst in the method of the present invention. In this case, the presence of said sulfur or/and said sulfur compound occasionally serve to control the direction for the nano-carbon materials to be grown.

The sulfur compound can include thiol, thioacetamide, thionaphthene, thiosemicarbazido, thiourea, and thiophene. Of these, thiol is particularly preferable.

As preferable specific examples of the thiol, there can be illustrated 1-octanethiol(n-octylmercaptan), 1-decanethiol (n-decylmercaptan), 1-dodecanethiol (n-dodecylmercaptan), n-butylmercaptan, propylmercaptan, methylmercaptan, ethylmercaptan, benzylmercaptan, and thiophenol.

The sulfur or the sulfur compound is not always necessary to be externally added. The sulfur or the sulfur compound may be one originally contained in the starting material. Particularly, some of those materials previously mentioned as the starting material often contain sulfur or/and sulfur compound therein. Such sulfur or/and such sulfur compound contained in the starting material may be used instead of the sulfur or/and the sulfur compound which are externally added.

The method of the present invention is preferred to include a heat-treating step (c). The reaction product obtained in the foregoing step (a) in the first embodiment of the process of the present invention or in the foregoing
5 step (b) in the second embodiment of the process of the present invention contains nano-carbon materials synthesized. The heat-treating step (c) serves to improve the purity of the nano-carbon materials of the reaction product by removing impurities including amorphous carbons contained therein
10 and it also serves to further develop the graphene sheet structures of the nano-carbon materials.

It is preferred that the reaction product prior to subjecting to the heat treatment or the heat-treated reaction product obtained in the heat-treating step (c) is washed with
15 an acid or the like to remove the catalyst (the catalyst particles) therefrom. By performing the heat treatment in the heat-treating step (c) at a temperature of more than 1500 °C, it is possible that the catalyst remained in the nano-carbon materials is removed by way of sublimation.

20 From a viewpoint of efficiently removing aforesaid impurities including amorphous carbons and also from a viewpoint of improving the purity of the nano-carbon materials, the heat treatment of the reaction product in the heat-treating step (c) is preferred to perform at a
25 temperature in a range of from 400 to 2800 °C. Similarly, the

heat treatment of the reaction product in the heat-treating step (c) is preferred to perform in a gas atmosphere composed of inert gas. The inert gas can include argon gas, helium gas and nitrogen gas. These gases may be used either singly or in
5 combination of two or more of them as a mixed gas.

In order to surely remove the impurities including amorphous carbons and in order to surely improve the purity of the nano-carbon materials, it is preferred that the heat treatment of the reaction product is repeated several
10 times by changing the heat-treating temperature, for instance, in such a manner that the reaction product is subjected to a first heat treatment at a temperature in a low temperature side region of the above-described temperature region, followed by subjecting to a second heat treatment at
15 a temperature in a middle to high temperature side region of the above-described temperature region.

To be more specific, in order to desirably develop the graphene sheet structures of the nano-carbon materials while surely removing the impurities including amorphous carbons
20 to improve the crystallinity of the nano-carbon materials, it is preferred that the reaction product is subjected to a first heat treatment at a relatively low temperature in a range of from 400 to 800 °C, followed by subjecting to a second heat treatment at a high temperature in a range of
25 from 900 to 2800 °C, and it is more preferred that the

reaction product is subjected to a first heat treatment at a relatively low temperature in a range of from 400 to 800 °C, followed by subjecting to a second heat treatment at a high temperature in a range of from 1000 to 2200 °C.

5 Separately, the heat treatment of the reaction product at a temperature in a region of from 2200 to 2800 °C is liable to develop the graphite structures (comprising a plurality of graphene sheets stacked) of the nano-carbon materials contained therein.

10 In the case where the heat treatment of the reaction product is repeated several times in this way, in order to improve the effect of the heat treatment for the reaction product, it is possible to adopt a manner in that the heat-treated reaction product obtained, for instance, in
15 the first heat treatment is pulverized prior to subjecting to the next heat treatment.

 The nano-carbon materials synthesized according to the method of the present invention are somewhat different depending the related conditions including the kind of the
20 starting material used, the kind of the catalyst used, the kind of the supplementary material as the reaction promotion medium used to form a supercritical fluid or a subcritical fluid to be contacted with the starting material, and the temperature and the pressure adopted in
25 the synthesis reaction.

However, the nano-carbon materials produced according to the method of the present invention include nano-carbon materials comprising such aggregates as below-mentioned which are identified by a scanning
5 electron microscope (SEM). Particularly, the nano-carbon materials produced according to the method of the present invention typically include nano-carbon materials comprising aggregates of a plurality of filament-like shaped (or worm-like shaped) microunits, and nano-carbon materials
10 comprising aggregates of a plurality of tube-like shaped microunits, wherein the microunits in each case have an average diameter in a range of from 4 to 400 nm and an average length in a range of from 100 to 10000 nm. In the method of the present invention, these filament-like (or
15 worm-like) or tube-like nano-carbons are likely to be synthesized at a high purity and at a high yield.

The diameters of these nonocarbon materials are liable to depend on the average particle size of a powdery catalyst used as the catalyst in the method of the present
20 invention.

According to observation by a transmission electron microscope (TEM) with respect to aforesaid microunits, the nano-carbon materials produced according to the method of the present invention include (a) nano-carbon materials
25 having a microstructure in that a plurality of graphene

5 sheets shaped in a cup-like or megaphone-like form which are stacked and developed into a filament-like state, (b) nano-carbon materials having a microstructure in that a graphene sheet is wound in a lengthwise direction parallel to a fiber axis into a single-layered tubular form or wound several times in a lengthwise direction slant to a fiber axis into a multi-layered tubular form, (c) nano-carbon materials comprising a platelet type graphite nanofiber in which a plurality of graphene sheets are stacked vertically to a fiber axis or a herring-bone type graphite nanofiber in which a plurality of graphene sheets are stacked slantingly to a fiber axis, and (d) nano-carbon materials having a microstructure in that a graphene sheet is developed into a sphere form or a disk form.

The nano-carbon materials described in the above (a) to (c) have a diameter in a range of from 4 to 400 nm and have a diameter in a range of from 20 to 400 nm in many cases.

20 In the method of the present invention, it is liable that filament-like (or worm-like) or tube-like nano-carbons having such microstructure as described in the above (a) or (b) are readily synthesized at a high purity and at a high yield, and said nano-carbons having such microstructure as described in the above (a) are more likely to be synthesized.

In the case where a given transition metal element-containing material is used as the catalyst, it is considered that in many cases, the growth of those nano-carbon materials mentioned in the above is initiated from the starting point based on the transition metal element-containing material. Therefore, the synthesized nano-carbon materials contain a transition metal or a transition metal compound resulted from the catalyst at their tip portions in many cases. Such transition metal or transition metal compound can be removed by dissolving it with an acid or the like. In the alternative, such residual transition metal or transition metal compound can be removed by way of heat treatment at a temperature of more than 1500 °C.

The method of the present invention is preferred to have a purification step (d) after the heat-treating step (c).

In the case where as the transition metal element-containing material as the catalyst, for instance, a magnetic transition metal selected from the group consisting of Fe, Ni, and Co or a magnetic transition metal compound whose transition metal element is selected from these magnetic transition metal element is used, the resulting nano-carbon materials-containing reaction product contains a magnetic body comprising such magnetic transition metal element.

The reaction product is heat-treated in the

heat-treating step (c) in the manner as previously described. The purification step (d) comprises subjecting the heat-treated reaction product to a purification treatment of collecting only the magnetic body-containing

5 nano-carbon materials by means of a magnet such as a permanent magnet or an electromagnet to obtain a purified nano-carbon materials-containing product. To be more specific, said heat-treated reaction product is dispersed in a dispersion medium such as alcohol or water while
10 irradiating ultrasonic wave, and thereafter, the magnetic body-containing nano-carbon materials are collected by means of a permanent magnet or an electromagnet, whereby it is possible to obtain a purified nano-carbon materials-containing product.

15 In the case where the purified nano-carbon materials-containing product still contain a residue resulted from the foregoing transition metal or transition metal compound, it is possible to adopt a further purification step wherein the product is treated with an
20 acid (such as nitric acid, hydrochloric acid, sulfuric acid, or hydrofluoric acid) or an alkali (such as sodium hydroxide or potassium hydroxide) to dissolve and remove the residue and the product thus treated is washed and dried. By this, it is possible to obtain a surely purified nano-carbon
25 materials-containing product.

Separately, the purification step (d) may be performed in the following manner. In the case where the nano-carbon materials-containing product having been heat-treated in the heat-treating step (c) contain a transition metal or a transition metal compound resulted from the catalyst, the product is treated with an acid (such as nitric acid, hydrochloric acid, sulfuric acid, or hydrofluoric acid) or an alkali (such as sodium hydroxide or potassium hydroxide) to dissolve and remove the transition metal or the transition metal compound contained in the nano-carbon materials-containing product and the product thus treated is washed and dried. By this, it is possible to obtain a purified nano-carbon materials-containing product which contains neither the transition metal nor the transition metal compound.

However, there is an occasion in that it is preferred for the nano-carbon materials obtained to contain such residue resulted from the catalyst in their microunits or in their tip portions, depending on the application use. In this case, the purification by means of said acid or said alkali is not necessary to be performed. However, in the case where the nanocarbon materials are adopted in the application use where said residue contained in the nano-carbon materials is liable to provide adverse effects, it is preferred that said purification is performed.

Separately, in both the purification by means of the magnet and the purification by means of the acid or the alkali, in order to improve the efficiency of the purification, when the nonocarbon materials-containing product is pulverize by
5 means of a mill prior to the purification treatment, intertwined aggregates of nano-carbons can be unraveled and this more improves the purification efficiency.

FIG. 1 shows a flow chart illustrating an example of the above-described method of the present invention.
10 FIG. 2 is a schematic diagram illustrating an example of a reaction apparatus used for practicing the method of the present invention.

Description will be made with reference to FIG.1.

In Step 1, a given starting material, a given
15 catalyst, and if necessary, a given reaction promotion medium (comprising a supplementary material capable of functioning to promote the reaction of said starting material) and given inert gas are introduced into a substantially enclosed reaction vessel (which is deoxidized) of a reaction
20 apparatus.

In Step 2, the materials introduced in the reaction vessel are together heat-treated for a prescribed period of time at a temperature in a range of from 100 °C to 800 °C while being compressed at a pressure in a range of from
25 0.2 MPa to 60 MPa, whereby the starting material and/or

the reaction promotion medium is converted into a supercritical fluid or a subcritical fluid and the starting material is reacted to obtain a reaction product containing nano-carbon materials, followed by removing.

5 unreacted starting material contained in the reaction product to obtain a nano-carbon product in Step 3.

In Step 4, the nano-carbon product obtained in Step 3 is subjected to a heat treatment at a temperature of 400 °C to 2800 °C preferably in an inert gas atmosphere mainly in
10 order to remove impurities (including amorphous carbons) contained in the nano-carbon product. If necessary, the heat-treated nano-carbon product is subjected to a purification treatment to remove the residual catalyst contained therein.

15 However, depending on the application use of the nano-carbon product, it is not always necessary to perform Step 3 or Step 4.

The reaction apparatus shown in FIG. 2 comprises a substantially enclosed pressure reaction vessel 200
20 provided with a heater 203, a pressure gauge 206, a safety vent 207, and an agitation mechanism 211. Reference numeral 201 indicates a starting material and/or a reaction promotion medium introduced in the reaction vessel 200, and reference numeral 202 indicates a catalyst. The reaction vessel 200 is
25 provided with a supply pipe 209 which is connected to a

starting material reservoir 204 and a reaction promotion medium reservoir 205 through valves as shown in FIG. 2. The reaction vessel 200 is also provided with an exhaust pipe 210 which is connected to a vacuum pump 208 through a valve as
5 shown in FIG. 2.

At least the inner wall of the reaction vessel 200 is made of preferably a stainless steel or more preferably a Ni-Mo alloy so as to have sufficient corrosion resistance.

Although not shown in FIG. 2, the reaction apparatus
10 is preferred to have a circulating flow reaction system in that from the reaction product containing nano-carbon materials and unreacted starting material which are outputted from the reaction vessel, a nano-carbon materials-containing reaction product is separated and the
15 unreacted starting material is returned into the reaction vessel, in order to improve the yield from the starting material.

The production of a nano-carbon product using the reaction apparatus shown in FIG. 2 is performed, for instance,
20 as will be described below.

A given catalyst 202 is introduced in the reaction vessel 200 and the inside of the reaction vessel 200 is evacuated to deoxidize through the exhaust pipe 210 by actuating the vacuum pump 208. Then, a prescribed amount of
25 a given starting material from the starting material

reservoir 204 is introduced in the reaction vessel 200 through the supply pipe 209. At this time, if necessary, a prescribed amount of a given reaction promotion medium such as carbon dioxide or the like from the reaction promotion medium
5 reservoir 205 is also introduced in the reaction vessel 200 through the supply pipe 209. The materials (the catalyst, the starting material, and the reaction promotion medium) in the reaction vessel 200 are subjected to a heat treatment at a prescribed temperature (which exceeds the critical point
10 where the starting material or the reaction promotion medium is converted into a supercritical fluid or a subcritical fluid) by actuating the heater 203 while being compressed at a prescribed pressure and while agitating said materials by means of the agitation mechanism 211 so
15 that the starting material 201 is uniformly contacted with the catalyst 202, whereby nano-carbon materials are synthesized from the starting material.

FIG. 3 is a schematic diagram illustrating an example of a reaction apparatus for continuously producing
20 nano-carbon materials in accordance with the method of the present invention. In FIG. 3, reference numeral 300 indicates a substantially enclosed pressure reaction vessel provided with a supply means for supplying a starting material 304 into the reaction vessel 300, a supply means for supplying a
25 catalyst 305 into the reaction vessel 300, and a supply

means for supplying a reaction promotion medium 306 into the reaction 300. The reaction promotion medium 306 is supplied, if required. Reference numeral 301 indicates a separator for separating a product (a nano-carbon product).

5 Reference numeral 302 indicates a recovery and purification tower for recovering and purifying a starting material. Reference numeral 303 indicates a compressor, and reference numeral 307 indicates a nano-carbon product outputted from the separator 301, collected in a receiving vessel.

10 The continuous production of nano-carbon materials in the apparatus shown in FIG. 3 is performed, for instance, as will be described below.

After the inside of the reaction vessel 300 is sufficiently deoxidized, a given starting material 304 and
15 a given catalyst 305, and if necessary, a given reaction promotion medium 306 are introduced into the reaction vessel 300. The materials (the starting material 304, the catalyst 305 and the reaction promotion medium 306) in the reaction vessel 300 are subjected to a heat treatment at a prescribed
20 temperature (which exceeds the critical point where the starting material or the reaction promotion medium is converted into a supercritical fluid or a subcritical fluid) while being compressed at a prescribed pressure and while agitating said materials so that the starting material
25 304 is uniformly contacted with the catalyst 305, whereby

nano-carbon materials are synthesized from the starting material. A mixture comprising a nano-carbon materials-containing product and unreacted starting material which is outputted from the reaction vessel 300 is transported
5 into the separator 301, where the nano-carbon materials-containing product (307) is separated from the unreacted starting material (304), the nano-carbon materials-containing product 307 is sent to the receiving vessel. The unreacted starting material (304) which is
10 outputted from the reaction vessel 300 is transported into the recovery and purification tower 302, where the unreacted starting material (304) is purified into a pure starting material 304, which is followed by being transported into the reaction vessel 300 through the compressor 303. Following
15 this, the above procedures for synthesizing nano-carbon materials are repeated to produce a nano-carbon materials-containing product, which is collected in the receiving vessel.

By the way, the formation of a nano-carbon material
20 synthesized by the method of the present invention can be identified by way of observation by means of a scanning electron microscope (SEM), and the microstructure of said nano-carbon material can be identified by way of observation by means of a transmission electron microscope (TEM).

25 The proportion of an amorphous component contained in

the nano-carbon material may be analyzed by means of X-ray diffraction analysis or laser Raman spectroscopy. In the case where a nano-carbon material synthesized contains a carbon nanotube, in the Raman spectrum of said carbon nanotube, there are observed a Raman line at a position in the vicinity of 1528 to 1606 cm^{-1} and a Raman line at a position in the vicinity of 1353 cm^{-1} . In the X-ray diffraction analysis, there is observed a sharp diffraction peak when the nano-carbon material is of a high purity. When the nonocarbon material contains an amorphous carbon in a large amount, there is observed a broad diffraction peak. In the Raman spectrum for this case, there is observed a large peak at a position in the vicinity of 1353 cm^{-1} .

Consequently, the purity of a nano-carbon material synthesized can be evaluated mainly by way of identification of the form thereof by means of SEM. Besides, it can be also evaluated on the basis of the observed result by TEM, the half band width of an X-ray diffraction peak, or the ratio of a peak intensity at a position in the vicinity of 1353 cm^{-1} to that at a position in the vicinity of 1528 to 1606 cm^{-1} in the Raman spectrum.

Separately, evaluation with respect to the performance of a nano-carbon materials-containing product obtained in the present invention when it is used as an anode material for a rechargeable lithium battery may be performed,

for instance, in the following manner. A cell is prepared by arranging a working electrode comprising said nano-carbon materials-containing product and a counter electrode comprising a lithium metal in an electrolyte solution comprising a lithium salt as an electrolyte dissolved in a nonaqueous solvent such that said working electrode and said counter electrode are opposed to each other. Then, lithium is electrochemically inserted in the working electrode and the lithium is electrochemically released from the working electrode, where the quantity of electric current flown upon the insertion of the lithium is compared with that upon the release of the lithium. When both the former quantity and the latter quantity are large and a difference between the former quantity and the latter quantity is small so as to be close to zero, it means that the performance of the nano-carbon materials-containing product as the anode material for a rechargeable lithium battery is excellent.

Evaluation with respect to the performance of a nano-carbon materials-containing product obtained in the present invention when it is used as a cathode for a field emission display (FED) may be performed, for instance, in the following manner. A prescribed electric field is applied between a cathode comprising said nano-carbon materials-containing product and an anode as the counter

electrode to said cathode under reduced pressure, where the value of an electric current flown per a unit area of the cathode is measured.

When the electric current value is large, it means
5 that the nano-carbon materials-containing product is excellent in terms of the performance as the cathode for the FED.

Evaluation with respect to the hydrogen storage ability of a nano-carbon materials-containing product obtained in the present invention to store hydrogen
10 therein may be performed, for instance, in the following manner. Said nano-carbon materials-containing product is maintained in a hydrogen gas under low temperature condition to permeate hydrogen gas in the nano-carbon materials-containing product and thereafter, the nano-carbon
15 materials-containing product is heated to release hydrogen from the product, where the amount of the permeated hydrogen and the amount of the released hydrogen are measured. Based on the measured results, the stored hydrogen amount per a unit weight of the product is computed.
20 When said amount is large, it means that the nano-carbon materials-containing product is good enough in the hydrogen storage ability.

In order to evaluate the performance of a nano-carbon materials-containing product obtained in the
25 present invention when it is used in a

catalyst-retaining layer of Pt or the like in a fuel cell, the specific surface area and the electron conductivity of the nano-carbon materials-containing product are important factors. Therefore, said specific surface area and said
5 electron conductivity are measured. Besides, the average particle size of catalyst particles of Pt or the like which are retained in the nano-carbon materials-containing product and the power output characteristics of a fuel cell in which a catalyst-retaining layer comprising the nano-carbon
10 materials-containing product having catalyst particles of Pt or the like retained therein is used are evaluated. In this case, it is better that the specific surface area is high, the resistivity is small, and the average particle size of the catalyst particles which are retained is small. When the
15 resistivity is small, the electron conductivity is increased and the electrode resistance is decreased, and as a result, the power outputted is increased.

A nano-carbon materials-containing product obtained in the present invention can be desirably used, for instance,
20 as an electrode material of a rechargeable lithium battery, as a cathode material of a FED, and as a catalyst-retaining layer of a fuel cell.

In the following, description will be made of the usage of a nano-carbon materials-containing product
25 (hereinafter simply referred to as "nano-carbon material")

obtained in the present invention in such applications.

Rechargeable Lithium Battery:

In the case where the nano-carbon material is used in a rechargeable lithium battery (here, this includes a
5 rechargeable lithium ion battery), it is preferred to be used as an anode material to store and release lithium ion, as an electrically conductive auxiliary for an anode material, or as an electrically conductive auxiliary for a cathode to store and release lithium ion.

10 FIG. 4 is a schematic cross-sectional view illustrating the constitution of an example of a rechargeable lithium battery. In FIG. 4, reference numeral 401 indicates an anode, reference numeral 402 an ion conductor, reference numeral 403 a cathode, reference numeral 404 an anode
15 terminal, reference numeral 405 a cathode terminal, and reference numeral 406 a battery housing.

The anode 401 in the rechargeable lithium battery shown in FIG. 4 comprises an electrode structural body 505 shown in FIG. 5.

20 In the electrode structural body shown in FIG. 5, the nano-carbon material is used in the anode material which functions to store and release lithium ion.

In FIG. 5, reference numeral 500 indicate a collector, reference numeral 501 a nano-carbon material in a powdery form
25 (obtained in the present invention), reference numeral 502 a

binder, reference numeral 503 an electrically conductive auxiliary, and reference numeral 504 an active material layer.

By the way, in another electrode structural body (as an anode), in the case where instead of the nano-carbon material 501, Si, Sn or an alloy thereof is used in the anode
5 material to store and release lithium ion, it is possible to use a nano-carbon material obtained in the present invention as the electrically conductive auxiliary 503 because the nano-carbon material is of a small average
10 particle size and is highly electrically conductive.

The electrode structural body 505 shown in FIG. 5 may be prepared, for instance, in the following manner.

A binder 502 comprising an organic polymer is admixed with aforesaid nano-carbon material 501, and if necessary,
15 an electrically conductive auxiliary 503 and a solvent are added, to obtain a mixture. The mixture is disposed on a collector 500 comprising a copper foil or the like to form an active material layer 504 on the collector 500, whereby an electrode structural body 505 is obtained.

20 The resultant electrode structural body 505 is used as the anode 401 in the rechargeable lithium battery shown in FIG. 4.

As aforesaid organic polymer used as the binder 502, it is possible to use a fluororesin such as polyvinylidene
25 fluoride or the like or a water-soluble organic polymer such

as polyvinyl alcohol or the like.

As the cathode 403 in the rechargeable lithium battery shown in FIG. 4, it is possible to use an electrode structural body prepared, for instance, in the following manner. A powder of a lithium-transition metal oxide, a lithium-transition metal phosphate, or a lithium-transition metal sulfate, an electrically conductive auxiliary comprising a graphite powder or the like, a binder comprising an organic polymer, and a solvent are mixed to obtain a mixture. The mixture is disposed on a collector comprising an aluminum foil or the like to form a cathode active material layer on the collector, whereby an electrode structural body is obtained. The resultant electrode structural body is used as the cathode 403. The transition metal element of said lithium-transition metal oxide, said lithium-transition metal phosphate or said lithium-transition metal sulfate which is used as the cathode active material may be Co, Ni, Mn, or Fe. Similarly, as said organic polymer used as the binder, it is possible to use a fluororesin such as polyvinylidene fluoride or the like or a water-soluble organic polymer such as polyvinyl alcohol or the like.

By the way, as the above-described electrically conductive auxiliary, it is possible to use a nano-carbon material obtained in the present invention because the nano-carbon material is of a small average particle size and

is highly electrically conductive. The electrode structural body as the cathode 403 in this case becomes to be of the same constitution as the electrode structural body shown in FIG. 5 except that 501 comprises a lithium-transition metal oxide or the like and the electrically conductive auxiliary 503 comprises said nano-carbon material.

As the ion conductor 402 arranged between the anode 401 and the cathode 403 in the rechargeable lithium battery shown in FIG. 4, it is possible to use a separator comprising a microporous polyolefin series film formed of polyethylene or polypropylene having an electrolyte retained therein.

The electrolyte may be an electrolyte solution obtained by dissolving a lithium salt selected from the group consisting of lithium salts of Li^+ (lithium ion) with Lewis acid ions such as BF_4^- , PF_6^- , AsF_6^- , ClO_4^- , CF_3SO_3^- , $\text{N}(\text{CF}_3\text{SO}_2)_2^-$, or BPh_4^- (with Ph being a phenyl group) in an organic solvent such as ethylene carbonate, propylene carbonate, dimethyl carbonate, or diethyl carbonate, or a gelled electrolyte obtain by gelating said electrolyte solution by adding an organic polymer thereto.

FED (field emission display):

FIG. 6 is a schematic cross-sectional view illustrating the constitution of an example of a FED.

In FIG. 6, reference numeral 600 indicates an insulating plate (a glass plate), reference numeral 601 a back

electrode (a cathode), reference numeral 602 a cathode layer formed using a nano-carbon material (obtained in the present invention), reference numeral 603 an insulating spacer (a barrier wall), reference numeral 604 a fluorescent substance layer, reference numeral 605 a transparent electrode (an anode), reference numeral 606 a surface mask, and reference numeral 607 a transparent surface member (comprising a glass plate).

The FED shown in FIG. 6 may be prepared, for instance, in the following manner. A metal electrode pattern 601 is arranged on a glass plate 600. On the metal electrode pattern 601, a paste obtained by mixing aforesaid nano-carbon material with a binder to obtain a mixture and adding a solvent to said mixture is coated by means of screen-printing or the like, followed by drying and baking to form a layer as the cathode layer 602. A transparent electrode pattern 605 is formed on a glass plate 607, and a fluorescent substance layer 604 is formed on the transparent electrode pattern 605 by means of screen-printing or the like. The transparent electrode 605 (the anode) and the cathode layer 602 are opposed to each other, and a spacer 603 (a barrier wall) is arranged between the transparent electrode 605 and the cathode layer 602. After the inside space of the system is evacuated to a prescribed vacuum, the system is closed. In this way, the FED shown in FIG. 6 may be prepared.

The I-V characteristics with respect to field emission from a nano-carbon material obtained in the present invention may be evaluated, for instance, in the following manner.

5 FIG. 7 is a schematic cross-sectional view illustrating the constitution of an example of an element used for evaluating the field emission performance of said nano-carbon material. In FIG. 7, reference numeral 700 indicates an insulating substrate, reference numeral 701 a
10 cathode pattern, reference numeral 702 a cathode layer formed using said nano-carbon material, reference numeral 703 an insulating spacer, reference numeral 704 an anode, reference numeral 705 a cathode lead, and reference numeral 706 an anode lead.

15 The element shown in FIG. 7 is placed in a vacuum chamber provided with a current introduction terminal, where the I-V characteristics with respect to field emission from the nano-carbon material may be evaluated by applying a prescribed voltage between the anode 704 and the cathode
20 702 (comprising the nano-carbon material) and measuring the value of an electric current flown between the cathode 702 and the anode 704.

 The element shown in FIG. 7 may be prepared, for instance, in the following manner. A mask having a cathode
25 pattern with an electrode-drawing portion formed by way of

etching is close-contacted onto a sodium-free glass substrate 700 (comprising, for instance, a No. 7059 glass plate produced by Corning Company), and thereafter, a 50 nm thick Cr film, a 300 nm thick Al film and a 50 nm thick Cr film are sequentially deposited by means of electron beam evaporation or the like to form a cathode pattern 701. Then, a nano-carbon material obtained in the present invention is dispersed in isopropyl alcohol while irradiating ultrasonic wave, and said cathode pattern and a counter electrode are immersed in the dispersion, where a D.C. electric field is applied between the cathode pattern 701 and the counter electrode to deposit said nano-carbon material on the cathode pattern 701 to form a cathode layer 702. Successively, an insulating member comprising a mica and having a thickness in a range of from about 20 to 200 μm as the insulating spacer 703 is fixed on the cathode layer 702, and thereon, an aluminum plate as the anode 704 is fixed. Thereafter, a cathode lead 705 is connected to the Cr/Al/Cr film as the cathode pattern 701, and an anode lead 706 is connected to the aluminum plate as the anode 704. In this way, the element shown in FIG. 7 may be prepared.

The evaluation of the I-V characteristics with respect to field emission of the nano-carbon material by using the element shown in FIG. 7 may be performed in the

following manner. The element is placed in a vacuum chamber provided with a current introduction terminal and which is preferably maintained at a vacuum of less than 10^{-3} Pa, where a prescribed voltage is applied between the anode lead 706 and the cathode lead 705 and the value of an electric current flown between the cathode 702 and the anode 704 is measured, wherein based on the interrelation between the values of the flown electric current and the values of the voltage applied, the I-V characteristics of the nano-carbon material are evaluated.

Hydrogen Storage Material:

The hydrogen-storing performance of a nano-carbon material produced in the present invention may be evaluated by using an appropriate measuring apparatus as shown in FIG. 8. The measuring apparatus shown in FIG. 8 has a container with a prescribed volume in which said nano-carbon material is charged and a vessel in which hydrogen is stored, wherein said container and said vessel are connected through a switching valve.

In FIG. 8, reference numeral 800 indicates a high pressure hydrogen gas cylinder, reference numeral 801 a vessel in which hydrogen is stored, reference numeral 802 a container in which the nano-carbon material is charged, reference numeral 803 a temperature controller, reference numeral 804 a vacuum pump, reference numeral 805 a pressure

gage, reference numeral 806 a vacuum gage, reference numeral 807 a pressure regulation valve, and each of reference numerals 808, 809, 810, 811, 812, and 813 a switching valve.

The vacuum gage 806 is connected to the container 802
5 through the switching valves 811, 812 and 813. The vacuum pump 804 is connected to the container 802 through the switching valves 811 and 812. The pressure gage 805 is connected to the vessel 801 through the switching valve 809. The hydrogen gas cylinder 800 is connected to the vessel 801 through the
10 switching valve 808 and the pressure regulating valve 807.

The evaluation of the hydrogen-storing performance of the nano-carbon material by using the measuring apparatus shown in FIG. 8 may be performed, for instance, in the following manner.

15 A nano-carbon material obtained in the present invention and which has been sufficiently dried is provided. The weight of the nano-carbon material is measured, and the nano-carbon material as an object to be measured is inserted in the container 802. The inside of the container 802 is
20 evacuated to a high vacuum by means of the vacuum pump 804, and hydrogen gas from the vessel 801 whose inside pressure is maintained at a prescribed pressure is introduced into the container 802 by opening the switching valves 810 and 811, and after a prescribed period of time is elapsed,
25 the hydrogen gas pressure in the container 802 and that in the

vessel 801 are measured.

From the initial hydrogen gas pressure in the vessel 801, the volume of the vessel 801 and that of the container 802, it is possible to compute the amount of hydrogen stored
5 in the nano-carbon material per a unit weight of the nano-carbon material. However, in practice, while changing the pressure of the hydrogen gas introduced into the container 802, the stored hydrogen amount and the released hydrogen amount respectively when the hydrogen gas pressure
10 in the container 802 is equilibrated are measured, and based on the measured results, the hydrogen stored amount per a unit weight of the nano-carbon material is computed.

In the following, the present invention will be described in more detail with reference to examples. It
15 should be understood that these examples are only for illustrative purposes and the scope of the present invention is not restricted by these examples.

Example 1

After the pressure reaction vessel made of a
20 Hastelloy (trademark name: comprising a Ni-Mo alloy, produced by Haynes International Inc.) with an inner volume of 95 ml of the reaction apparatus shown in FIG. 2 was evacuated to a prescribed vacuum by means of the vacuum pump, 2.5 g of n-hexane (the critical temperature: 234.4 °C;
25 the critical pressure: 2.97 MPa) as the starting material

and 0.2 g of a nickelocene (bis(cyclopentadienyl)nickel) as the catalyst were introduced into the reaction vessel, followed by adding 30 g of dry ice as the reaction promotion medium thereto, and the reaction vessel was closed, where
5 said dry ice was vaporized into CO₂ gas at room temperature and therefore, part of said CO₂ gas was exhausted outside the reaction vessel to adjust the inner pressure of the reaction vessel to a desired value. And the materials in the reaction vessel were subjected to reaction at a
10 temperature of 650 °C while being compressed at a pressure of 23 MPa and while agitating by means of the agitation mechanism for 2 hours, followed by being cooled to room temperature. Then, the reaction vessel was opened to take out a solid component, and the solid component is
15 dried to obtain 0.54 g of a reaction product in a powdery form, that is, a powdery nano-carbon product [this will be hereinafter referred to as "nano-carbon product (a)"].

A part of the nano-carbon product (a) was
20 subjected to a heat treatment at a temperature of 1500 °C in an argon gas atmosphere to obtain a powdery nano-carbon product (b). And a part of the nano-carbon product (b) was subjected to a heat treatment at a temperature of 2800 °C in an argon gas atmosphere to
25 obtain a powdery nano-carbon product (c).

Evaluation

Each of the nano-carbon product (a), the nano-carbon product (b) and the nano-carbon product (c) was evaluated by means of a scanning electron microscope (SEM) and a transmission electron microscope (TEM). In addition, each of them was evaluated by means of X-ray microanalysis, X-ray diffraction analysis and Raman spectroscopic analysis.

1. In the SEM observation of the nano-carbon product (a), there was obtained a SEM image shown in FIG. 9, showing that said SEM image substantially 100% comprises an enormous number of filament-like shaped microunits which are gathered. It was found that said filament-like shaped microunits have a diameter in a range of from about 10 nm to 100 nm, and they mostly have a length of less than about 4 μm but include longer ones whose length is more than 4 μm . It was also found that said filament-like microunits include ones whose outer diameter is about 87 μm and whose inner diameter (the diameter of a hollow portion) is about 30 nm.

In the X-ray microanalysis of the nano-carbon product (a), the presence of a residual nickel metal (resulted from the catalyst) at tips of said filament-like microunits was observed but the presence of other material than carbon was not observed. In the X-ray diffraction analysis of the nano-carbon product (a),

there were observed a diffraction peak based on graphite carbon and a diffraction peak based on nickel metal. From the results in the X-ray microanalysis and the X-ray diffraction analysis, it is considered that the nickelocene used as the catalyst was decomposed into a nickel metal during the reaction.

In the Raman spectroscopic analysis of the nano-carbon product (a), there were observed a relatively strong peak which is so-called a G-band near 1590 cm^{-1} and a relatively weak which is so-called a D-band near 1350 cm^{-1} . That is, for the relative peak intensity between the G-band peak near 1590 cm^{-1} and the D-band peak near 1350 cm^{-1} , it was found that the intensity of the former is stronger.

In the TEM observation of the nano-carbon product (a), there were obtained a TEM image (observed at a low magnification) shown in FIG. 10 and a TEM image (observed at a high magnification) shown in FIG. 11.

From FIG. 9 and FIG. 10 and also from the results in the X-ray microanalysis and the X-ray diffraction analysis, it is understood that the nano-carbon product (a) comprises nano-carbon materials having a hollow tubular structure grown from the surface of a nickel metal fine particle as schematically shown in FIG. 12.

FIGs. 13(a) to 13(e) are schematic views respectively illustrating a microstructure inferred from

a TEM image of a filament-like nano-carbon material. Particularly, FIG. 13(a) shows a microstructure in that a plurality of graphene sheets developed into a megaphone-like form are stacked and developed into a tubular form. FIG. 13(b) shows a microstructure in that a plurality of graphene sheets respectively developed into a cup-like form are stacked and developed into a pillar form. FIG. 13(c) shows a microstructure in that a plurality of graphene sheets are stacked vertically to a fiber axis and developed into a pillar form. FIG. 13(d) shows a microstructure in that a number of graphene sheets are stacked on a concentric circle in parallel to a fiber axis and developed into a tubular form. FIG. 13(e) shows a microstructure in that a number of graphene sheets are piled, concentrically wound while rotating in a fiber axis direction and developed into a tubular form.

From the TEM image shown in FIG. 11, it is considered that the nano-carbon product (a) would include filament-like nano-carbon materials having such a microstructure as shown in FIG. 13(a) or FIG. 13(e). In the TEM observation of a different sample of the nano-carbon product (a), there was observed a microstructure approximate to the microstructure shown in FIG. 13(b), and there was also observed another microstructure likely similar to the microstructure shown in FIG. 13(d).

2. For the nano-carbon product (b) [after having baked at 1500 °C] and the nano-carbon product (c) [after having baked at 2800 °C], it was found that such a microstructure as shown in FIG. 9 in that an enormous number of filament-like microunits are gathered is maintained in each of them.

In the Raman spectroscopic analysis of each of the nano-carbon product (b) and the nano-carbon product (c), there was observed substantially no distinct peak near 1350 cm^{-1} in the Raman spectrum. This means that the peak of 1350 cm^{-1} which was observed in the case of the nano-carbon product (a) was substantially disappeared due to the baking.

3. The foregoing procedures for the production of the nano-carbon product (a) were repeated to obtain a powdery nano-carbon product (a'). The nano-carbon product (a') was subjected to a heat treatment at a temperature of 1500 °C in an argon gas atmosphere to obtain a powdery nano-carbon product (b'). The nano-carbon product (b') was treated with hydrochloric acid then treated with nitric acid to elute and remove the residual nickel metal therein. The nano-carbon product (b') thus treated was washed with ion-exchanged water and heat-treated at a temperature of 350 °C in an air atmosphere, followed by being ground by means of a ball mill, to obtain a Ni-free nano-carbon powder [this will be hereinafter referred to as "nano-carbon powder (i)"].

A part of the nano-carbon powder (i) was subjected to evaluation of the I-V characteristics with respect to field emission in the following manner.

An element having such structure as shown in FIG. 7 was prepared in accordance with the previously described method for the preparation of the element shown in FIG. 7, except for the following points. That is, the nano-carbon powder (i) was dispersed in isopropyl alcohol while irradiating ultrasonic wave, and a cathode pattern formed of a stainless steel plate and a counter electrode are immersed in the dispersion, where a D.C. electric field is applied between the cathode pattern and the counter electrode to form a nano-carbon material layer as the cathode layer on the cathode pattern by way of cataphoresis, a 150 μm thick insulating member comprising a mica as the insulating spacer is fixed on the cathode layer, and thereon, an aluminum plate as the anode is fixed. In this way, there was prepared an element having such structure as shown in FIG. 7.

The element thus prepared was placed in a vacuum chamber provided with a current introduction terminal and which is maintained at a vacuum of less than 10^{-3} Pa, where a prescribed electric field was impressed to the element to measure I-V characteristics with respect to field emission. As a result, the nano-carbon powder (i) was

found to have a threshold voltage of less than 5V/ μm and an electron emission current value which is greater by about 10 times that of a commercially available carbon multinanotube material (produced by The Honjo Chemical Corporation).

4. An electrode structural body having such configuration as shown in FIG. 5 was prepared in accordance the previously described method for the preparation of the electrode structural body shown in FIG. 5, except that the remaining part of the nano-carbon powder (i) obtained in the above 3 was used as the nano-carbon material 501. This electrode structural body was evaluated with respect to insertion-release performance of lithium ion in the following manner.

15 A separator was interposed between the electrode structural body and a counter electrode comprising a lithium metal which are arranged such that they are opposed to each other, said separator comprising a microporous polyethylene film and which is incorporated with an electrolyte solution
20 obtained by dissolving 1 mol/l of lithium tetrafluoroborate (LiBF_4) in a mixed solvent composed of ethylene carbonate and diethyl carbonate at a mixing ratio of 3 : 7. Using this, electrochemical insertion and release of lithium ion was performed. As a result, a quantity of lithium ion which
25 is 1.2 times that in the case of using an electrode formed

of a natural graphite could be stored in the electrode structural body. This indicates that in the case where a rechargeable lithium battery having such configuration as shown in FIG. 4 is fabricated using aforesaid electrode structural body as the anode, the resulting rechargeable lithium battery becomes to have a greater capacity than that of a rechargeable battery fabricated using an electrode formed of a natural graphite as the anode.

5 5. The nano-carbon product (a) was subjected to evaluation with respect the hydrogen-storing ability thereof in accordance with the previously described evaluation method using the measuring apparatus shown in FIG. 8. As a result, the nano-carbon product (a) was found to have a hydrogen-storing ability which is substantially the same as that of a commercially available multi-walled carbon nanotube.

Example 2

 In this example, there were provided two substantially enclosed pressure reaction vessels made of a Hastelloy (trademark name: comprising a Ni-Mo alloy, produced by Haynes International Inc.) with an inner volume of 95 ml as the pressure reaction vessel (200) of the reaction apparatus shown in FIG. 2. Separately using these two reaction vessels, the procedures of Example 1 for the production of the nano-carbon product (a) were repeated,

except that the reaction temperature and the reaction pressure were changed to 450 °C and 14 MPa respectively, and the reaction time was changed to 6 hours, to separately obtain a powdery nano-carbon product (i) in an amount of 0.40 g in one reaction vessel and a powdery nano-carbon product (ii) in an amount of 0.82 g in another reaction vessel. In this case, the oxygen content and the moisture content in the two reaction vessels were not precisely controlled so as to be substantially the same upon introducing the starting material, the catalyst and the dryice therein.

Now, it is considered that the history of the reaction vessel, and the oxygen content or/and the moisture content in the system would have influenced to this difference in terms of the yield. Separately, because the valence number of the constituent nickel of the nickelocene as the catalyst is liable to change depending on the preservation state of the nickelocene in an air atmosphere, it is also considered that the nickelocene would have received an influence of oxygen or moisture and this would have become to be a factor to differentiate the yield.

In the SEM observation of each of the nano-carbon product (i) and the nano-carbon product (ii), there was obtained a SEM image in that an enormous number of filament-like shaped (or worm-like shaped) microunits are

gathered. And it was found that said filament-like shaped microunits have a diameter in a range of from about 20 nm to 30 nm. In the TEM observation of each of the nano-carbon product (i) and the nano-carbon product (ii), there was
5 observed a microstructure approximate to the microstructure shown in FIG. 13(b).

Example 3

The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that the
10 reaction temperature was changed to 450 °C, the reaction time was changed to 6 hours, the reaction pressure was changed to a prescribed pressure value in a range of from 14 to 16 MPa (see, Table 1), and instead of the nickelocene as the catalyst, a nickel fine powder, a cobalt fine powder, a
15 nickel-retained silica powder, a nickel-retained alumina powder, a nickel-retained alumina powder, a palladium-retained alumina powder, and a nickel oxide powder were separately used, to obtain a powdery nano-carbon product for each of these catalysts.

20 The results of the SEM observation revealed that any of the nano-carbon products contains an enormous number of filament-like shaped nano-carbon microunits which are gathered.

The reaction pressure, the yield of the nano-carbon
25 product, the use amount of the catalyst, and the diameter

of the microunits in the nano-carbon product in each case where aforesaid nickel fine powder, aforesaid cobalt fine powder, aforesaid nickel-retained silica powder, or aforesaid nickel oxide powder was used are collectively
5 shown in Table 1. Only in the case of the cobalt fine powder, the use amount was made to be 1 g.

Here, the nickel fine powder used in this example comprises particles having a particle size in a range of from 0.5 to 1.0 μm and a specific surface area in a range of from
10 1.5 to 2.5 m^2/g .

The nickel-retained silica powder used in this example retains the nickel in a amount of 70 wt.%, has a primary particle size in a range of from 0.01 to 0.02 μm and a secondary particle size of about 20 μm , and has a specific
15 surface area in a range of from 30 to 40 m^2/g .

The nickel-retained alumina powder used in this example has a primary particle size of from 0.1 μm and a secondary particle size in a range of from 5 to 10 μm . The palladium-retained alumina powder used in this example
20 has a primary particle size of 0.01 μm and a secondary particle size in a range of from 20 to 30 μm .

Based on the results shown in Table 1, it was found that in the case where the nickel-retained silica powder whose nickel (transition metal) particles are considered to be
25 smallest among other catalyst particles is used, a nano-carbon

material containing filament-like shaped nano-carbon microunits whose diameter is the smallest among others.

In the case of the nano-carbon product synthesized in the presence of the nickel oxide as the catalyst, it was found that the filament-like shaped nano-carbon microunits contained therein has a filament length which is relatively short. And in this case, the result of the X-ray diffraction analysis revealed that the nickel oxide was reduced into a metallic nickel during the reaction. This indicates that the atmosphere during the reaction became to be a reduction atmosphere. It is considered that such reduction atmosphere is composed of hydrogen gas or carbon monoxide. It is considered that said hydrogen gas would be generated when the starting material is decomposed. It is considered that said carbon monoxide is probably generated due to the reaction of said hydrogen gas with the carbon dioxide or due to the reaction of the starting material with residual oxygen in the reaction vessel. Further, there is a probability in that said carbon monoxide will become to be a raw material for a nano-carbon material synthesized in the reaction vessel.

Separately, it was recognized that filament-like shaped nano-carbon microunits grown from nickel particles having a relatively large particle size have a relatively large diameter of about 100 μm and have a microstructure approximate to the microstructure shown in FIG. 13(c).

Example 4

The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that instead of the nickelocene as the catalyst, an iron fine powder was used, to obtain a nano-carbon product. The nano-carbon product obtained in this example was found to contain filament-like shaped nano-carbon microunits which are similar to those in Example 1.

Separately, the above procedures were repeated by changing the reaction temperature to 450 °C. In this case, an aimed nano-carbon product was not obtained. The results of the X-ray diffraction analysis revealed that the iron of the iron fine powder as the catalyst was converted into an iron oxide.

Example 5

The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that the reaction temperature was changed to 450 °C, the reaction time was changed to 6 hours, the reaction pressure was changed to a prescribed pressure value in a range of from 9.3 to 30.1 MPa (see, Table 2), and instead of the n-hexane as the starting material, n-pentane, n-heptane, n-octane, n-nanone, n-decane, hexadecane, 2,2,4-trimethylpentane, cyclohexane, 1-hexene, and n-octene were separately used, to obtain a powdery nano-carbon product for each of these hydrocarbons.

The results of the SEM observation revealed that

any of the nano-carbon products contains an enormous number of filament-like shaped nano-carbon microunits which are gathered.

5 The starting material, the reaction pressure, the yield of the nano-carbon product, and the diameter of the microunits in the nano-carbon product in each case are collectively shown in Table 2.

Example 6

10 The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that the reaction temperature was changed to 450 °C, the reaction pressure was changed to about 10 MPa, the reaction time was changed to 6 hours, and instead of the n-hexane as the starting material, ethanol, 1-butanol, and hexanol were
15 separately used, to obtain a powdery nano-carbon product for each of these materials as the starting material.

The results of the SEM observation revealed that any of the nano-carbon products obtained contains an enormous number of filament-like shaped nano-carbon
20 microunits which are gathered.

The starting material, the reaction pressure, the yield of the nano-carbon product, and the diameter of the microunits in the nano-carbon product in each case are collectively shown in Table 3.

25 As the results shown in Table 3 illustrate, it is

understood that a nano-carbon product was obtained from the 1-butanol at a yield which is similar to that in the case of using the n-hexane belonging to the hydrocarbon.

Example 7

5 The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that the reaction temperature was changed to 450 °C, the reaction pressure was changed to 20.9 MPa, the reaction time was changed to 6 hours, and instead of the nickelocene as the
10 catalyst, a catalyst prepared as will be described in the following was used, to obtain a powdery nano-carbon product.

 The results of the SEM observation revealed that the nano-carbon product obtained contains a number of
15 spherical-shaped nano-carbons having a diameter in a range of from 1 to 3 μm which are gathered. This is different from the nano-carbon products obtained in other examples.

 The catalyst used in this example was prepared as will be described below.

20 (1). 7.08 of cetyltriacylammoniumbromide as a surfactant was added to 63.72 g of toluene and heated to 70 °C to dissolve the surfactant in the toluene, then 0.1 g of nickel chloride ($\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$) was added and dissolved therein to obtain a solution.

25 (2). An aqueous solution of NaBH_4 (obtained by

dissolving 0.0476 g of NaBH_4 in 2.5 g of deionized water) was subjected to reaction by dropwise adding to the solution obtained in the above step (1) while stirring the solution by means of a homogenizer to obtain a suspension.

5 (3). The suspension obtained in the above step (2) was subjected to centrifugation, washed using toluene and acetone, subjected to centrifugation. The solvent was removed from the resultant, followed by drying to obtain a catalyst used in this example.

10

Example 8

1. The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that the reaction temperature was changed to 450 °C, the reaction pressure was changed to 2.4 MPa, the reaction time was
15 changed to 6 hours, and instead of the dryice as the reaction promotion medium, liquid nitrogen was used, to obtain a powdery nano-carbon product in an amount of 0.01 g.

Although the yield of the nano-carbon product was small, the results of the SEM observation revealed that the
20 nano-carbon product contains an enormous number of filament-like shaped nano-carbon microunits which are gathered.

2. The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that the
25 reaction temperature was changed to 450 °C, the reaction

pressure was changed to 7.5 MPa, the reaction time was changed to 6 hours, and instead of the dryice as the reaction promotion medium, argon gas was used, to obtain a powdery nano-carbon product in a tiny amount. However, the results of the SEM observation revealed that the nano-carbon product contains an enormous number of filament-like shaped nano-carbon microunits which are gathered.

3. The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except that the reaction temperature was changed to 450 °C, the reaction pressure was changed to 9.5 MPa, and the reaction time was changed to 6 hours, to obtain a powdery nano-carbon product in an amount of 0.51. The results of the SEM observation revealed that the nano-carbon product contains an enormous number of filament-like shaped nano-carbon microunits which are gathered.

From the results in the above three cases 1 to 3, the following facts are understood. (1) Even when the reaction pressure is made to be about 2 MPa, an aimed nano-carbon is synthesized. (2) In a viewpoint to produce a nano-carbon product at a high yield, as the reaction promotion medium, carbon dioxide is more preferable than nitrogen gas or argon gas. Further, the results in the above three cases 1 to 3 indicate that carbon dioxide functions as a medium to promote

the synthesis reaction to synthesize a nano-carbon material, and they suggest a probability in that carbon dioxide contributes to the formation of a reduction atmosphere generated during the reaction and functions as a raw material for a nano-carbon material synthesized in the reaction vessel.

Example 9

1. Into the pressure reaction vessel made of a Hastelloy (trademark name: comprising a Ni-Mo alloy, produced by Haynes International Inc.) with an inner volume of 95 ml of the reaction apparatus shown in FIG. 2, 0.2 g of a silica powder having nickel particles in an amount of 70 wt.% retained therein as the catalyst was introduced. After this, the reaction vessel was evacuated to a prescribed vacuum by means of the vacuum pump, followed by introducing 7.26 g of n-hexane as the starting material and 11.26 g of carbon dioxide as the reaction promotion medium into the reaction vessel. The materials (the starting material, the catalyst and the reaction promotion medium) in the reaction vessel were subjected to reaction by heating them at 450 °C while being compressed at a pressure of 19.0 MPa and while agitating by means of the agitation mechanism for 6 hours, followed by being cooled to room temperature. Then, the reaction vessel was opened to take out a solid component, and the solid component is dried to obtain a powdery nano-carbon product in an amount of 2.36

g.

2. The procedures in the above 1 for the production of said nano-carbon product were repeated, except that instead of the n-hexane as the starting material, methane, ethane, propane, ethylene, and propylene were separately used, and the reaction pressure was changed to a prescribed pressure value in a range of from 9.15 to 11.04 (see, Table 4), to obtain a nano-carbon product for each of said hydrocarbons.

The results of the SEM observation revealed that any of the nano-carbon products obtained in the above two cases 1 and 2 contains an enormous number of filament-like shaped nano-carbon microunits which are gathered. And it was found that the filament-like shaped nano-carbon microunits have a diameter in a range of from 20 to 80 nm in the case where ethylene or propylene was used as the starting material.

The use amount of the starting material, the use amount of the carbon dioxide, the reaction pressure, and the yield of the nano-carbon product in each case are collectively shown in Table 4.

As Table 4 illustrates, it is understood that of n-hexane, ethylene and propylene used as the starting material, with respect to the conversion efficiency into a nano-carbon material, propylene is the highest, the second is ethylene, and the third is n-hexane. Particularly, in the

production method of the present invention, it is considered that unsaturated hydrocarbons are more liable to convert into a nano-carbon material having filament-like shaped microunits.

5 Separately, the nickel-retained silica powder used as the catalyst in this example is more stable in comparison with the nickelocene and it hardly receive an influence of residual oxygen in the reaction vessel, being different from the nickelocene. Therefore, it is considered that such
10 difference in terms of the yield as described in Example 2 would not have occurred in this example.

Example 10

Into the pressure reaction vessel made of a Hastelloy (Ni-Co alloy) with an inner volume of 95 ml of
15 the reaction apparatus shown in FIG. 2, 0.2 g of a ferrocene as the catalyst was introduced. After this, the reaction vessel was evacuated to a prescribed vacuum by means of the vacuum pump, followed by introducing 7.92 g of n-hexane as the starting material into the reaction vessel, and the
20 reaction vessel was closed. Then, the materials (said n-hexane and said ferrocene) in the reaction vessel were subjected to reaction by heating the materials in the reaction vessel at 800 °C while being compressed at a pressure of 2.1 MPa and while agitating by means of the
25 agitation mechanism for 2 hours, followed by being

cooled to room temperature. Then, the reaction vessel was opened to take out a solid component, and the solid component is dried to obtain a powdery nano-carbon product in an amount of 0.314 g.

5 In the TEM observation of the resultant nano-carbon product, there was obtained a TEM image shown in FIG. 14. Based on the TEM image shown in FIG. 14, it was found that said nano-carbon product has a microstructure in that a number of graphene sheets containing iron catalyst fine
10 particles are stacked, which is similar to the microstructure shown in FIG. 13(d).

Example 11

Into the pressure reaction vessel made of a Hastelloy (Ni-Co alloy) with an inner volume of 95 ml of
15 the reaction apparatus shown in FIG. 2, 0.2 g of a ferrocene as the catalyst was introduced. After this, the reaction vessel was evacuated to a prescribed vacuum by means of the vacuum pump, followed by introducing 3.89 g of methane as the starting material into the reaction vessel, and the
20 reaction vessel was closed. Then the materials (the starting material and the catalyst) in the reaction vessel were subjected to reaction by heating the materials in the reaction vessel at 800 °C while being compressed at a pressure of 12.9 MPa and while agitating by means of the
25 agitation mechanism for 10 minutes, followed by being

cooled to room temperature. Then, the reaction vessel was opened to take out a solid component, and the solid component is dried to obtain a powdery nano-carbon product in an amount of 0.447 g.

5 In the SEM observation of the resultant nano-carbon product, there was obtained a SEM image shown in FIG. 15. Based on the SEM image shown in FIG. 15, it was found that the nano-carbon product contains an enormous number of filament-like shaped nano-carbon microunits having a
10 diameter in a range of from 20 nm to 100 nm and a length in a range of from 30 to 100 μ m which are gathered. Separately, the results of the TEM observation revealed that the nano-carbon product has a carbon nanotube microstructure comprising a multi-walled tube.

15 The nano-carbon product obtained in this example was subjected to evaluation of the I-V characteristics with respect to field emission in the following manner.

 An element having such structure as shown in FIG. 7 was prepared in accordance with the previously described
20 method for the preparation of the element shown in FIG. 7, except for the following points. That is, the nano-carbon product was ground by means of a ball mill to obtain a nano-carbon fine powder. The nano-carbon fine powder was dispersed in isopropyl alcohol while irradiating ultrasonic
25 wave to obtain a dispersion. And a cathode pattern and

a counterelectrode were immersed in the dispersion, where a D.C. electric field was applied between the cathode pattern and the counter electrode to form a nano-carbon material layer as the cathode layer on the cathode pattern by way of cataphoresis, a 150 μm thick insulating member comprising a mica as the insulating spacer was fixed on the cathode layer, and thereon, an aluminum plate as the anode was fixed. In this way, there was prepared an element having such structure as shown in FIG.

10 7.

The element thus prepared was placed in a vacuum chamber provided with a current introduction terminal and which is maintained at a vacuum of less than 10^{-3} Pa, where a prescribed electric field was applied to the element to measure I-V characteristics with respect to field emission. As a result, the nano-carbon product obtained in this example was found to have a threshold voltage of less than 2 V/ μm and an electron emission current value which is greater by about 30 times that of a commercially available carbon multitanotube material (produced by The Honjo Chemical Corporation).

20

Example 12

Into the pressure reaction vessel made of a Hastelloy (Ni-Co alloy) with an inner volume of 95 ml of the reaction apparatus shown in FIG. 2, 0.2 g of a ferrocene

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as the catalyst was introduced. After this, the reaction vessel was evacuated to a prescribed vacuum by means of the vacuum pump, followed by introducing 9.34 g of propylene as the starting material into the reaction vessel, and the reaction vessel was closed. Then, the materials (the starting material and the catalyst) in the reaction vessel were subjected to reaction by heating the materials in the reaction vessel at 800 °C while being compressed at a pressure of 2.2 MPa and while agitating by means of the agitation mechanism for 5 minutes, followed by being cooled to room temperature. Then, the reaction vessel was opened to take out a solid component, and the solid component is dried to obtain a powdery nano-carbon product in an amount of 0.443 g.

In the SEM observation of the resultant nano-carbon product, there was obtained a SEM image shown in FIG. 16. Based on the SEM image shown in FIG. 16, it was found that the nano-carbon product contains an enormous number of filament-like shaped nano-carbon microunits having a diameter of less than 40 nm which are gathered. Separately, the results of the TEM observation revealed that the nano-carbon product has a carbon nanotube microstructure comprising a multi-walled tube.

Example 13

Into the pressure reaction vessel made of a

Hastelloy (Ni-Co alloy) with an inner volume of 95 ml of the reaction apparatus shown in FIG. 2, 0.2 g of a ferrocene as the catalyst was introduced. After this, the reaction vessel was evacuated to a prescribed vacuum by means of the vacuum pump, followed by introducing 3.89 g of methane as the starting material and 5.99 g of nitrogen (N_2) as the reaction promotion medium into the reaction vessel, and the reaction vessel was closed. Then, the materials (the starting material, the catalyst and the reaction promotion medium) in the reaction vessel were subjected to reaction by heating the materials in the reaction vessel at 800 °C while being compressed at a pressure of 16.0 MPa and while agitating by means of the agitation mechanism for 10 minutes, followed by being cooled to room temperature. Then, the reaction vessel was opened to take out a solid component, and the solid component is dried to obtain a powdery nano-carbon product in an amount which is 1.3 times that of the nano-carbon product in Example 11.

The results in the SEM observation of the resultant nano-carbon product revealed that the nano-carbon product obtained in this example contains an enormous number of filament-like shaped nano-carbon microunits having an average diameter of about 100 nm which are gathered. Here, it was found that in comparison of the nano-carbon microunits in this example with the nano-carbon microunits in

Example 11, the diameter of the former is greater than that of the latter, the distribution uniformity of the former is superior to that of the latter, and the length of the former is shorter than that of the latter.

5

Comparative Example 1

The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except for changing the reaction temperature to 90 °C and the reaction pressure to 15 MPa. In this case, a desired powdery nano-carbon could not be produced as in Example 1.

10

Comparative Example 2

The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except for changing the reaction pressure to 1 MPa. In this case, a desired powdery nano-carbon could not be produced as in Example 1.

15

Comparative Example 3

The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except for not introducing the nickelocene as the catalyst into the reaction vessel. In this case, a desired powdery nano-carbon could not be produced as in Example 1.

20

Comparative Example 4

The procedures of Example 1 for the production of the nano-carbon product (a) were repeated, except for

25

changing the n-hexane as the starting material to methanol. In this case, a desired powdery nano-carbon could not be produced as in Example 1.

Table 1

samples in Example 3	catalyst	amount of catalyst(g)	pressure(MPa)	yield(g)	diameter of nano-carbon microunit(nm)
A	Ni	0.2	14.7	0.86	20~100
B	Co	1.0	17.5	1.35	26~53
C	Ni/SiO ₂	0.2	16.6	0.56	7~27
D	NiO	0.2	15.7	0.718	20~30

Table 2

samples in Example 5	starting material	pressure(MPa)	yield(g)	diameter of nano-carbon microunit(nm)
A	n-pentane	30.1	0.187	not measured
B	n-heptane	23.7	0.45	not measured
C	n-octane	14.3	0.44	not measured
D	n-nonane	17.3	0.47	15-20
E	n-decane	14.6	0.69	not measured
F	hexadecane	15.4	0.53	15~30
G	2,2,4-trimethylpentane	14.8	0.52	not measured
H	cyclohexane	9.3	0.24	20~30
I	1-hexene	17.9	0.57	not measured
J	n-octene	18.2	0.69	not measured

Table 3

samples in Example 6	starting material	pressure(MPa)	yield(g)	diameter of nano-carbon microunit (nm)
A	ethanol	12.5	0.04	not measured
B	1-butanol	11.6	0.49	15~30
C	hexanol	15.9	0.01	not measured

Table 4

samples in Example 9	starting material	amount of starting material	amount of CO ₂	pressure(MPa)	yield(g)
A	n-hexane	7.26	11.26	19.0	2.36
B	methane	4.67	10.61	21.7	0.32
C	ethane	7.25	10.84	26.1	1.33
D	propane	7.16	9.15	22.1	2.08
E	ethylene	6.5	10.46	19.5	2.59
F	propylene	9.35	11.04	25.7	4.40